

Thermochemical evaluation of biochars properties from Portuguese agro-forestry residues for solid fuel applications

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1 **Title:**
2 **Thermochemical Evaluation of Biochars Properties from Portuguese**
3 **Agro-Forestry Residues for Solid Fuel Applications**

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15 **Abstract:** This study provides a high-quality comparative characterization
16 of biochars derived from regionally significant Portuguese feedstocks:
17 hazelnut shell, pine, pinecone, oak pruning waste, and swine manure. All
18 feedstocks were subjected to pyrolysis at 450 °C to evaluate their potential
19 as solid fuels. The results demonstrate the clear superiority of woody-based
20 biochars for energy applications, with hazelnut shell biochar exhibiting the
21 highest fixed carbon (up to 82.89%) and the highest lower heating value
22 (up to 31.64 MJ/kg). In contrast, swine manure biochar proved unsuitable
23 as a standalone fuel due to its extremely high ash content (48.34%). A
24 notable preliminary finding, based on a single case study, was the
25 significant improvement in carbon content in a slow-cooled hazelnut
26 sample, suggesting that post-pyrolysis conditions are not chemically inert
27 and offer a promising avenue for future research in biochar optimization.
28 This work highlights a hierarchical valorisation model for local biomass,
29 classifying feedstocks for optimal use in premium fuel production, general
30 energy applications, or soil amendment based on their distinct
31 thermochemical properties.

32 **Keywords:** Biochar; Pyrolysis; Energy density; Fixed carbon; Heating
33 value; Biomass residues

34

35

36 **1. Introduction**

37 The need for more sustainable energy sources and the urgency of
38 mitigating climate change have intensified research on the thermochemical
39 conversion of biomass [1–4]. Biomass valorisation is aligned with
40 decarbonisation goals, circular economy strategies, and the reduction of
41 waste disposal liabilities [5].

42 Among the available thermochemical routes, pyrolysis — the thermal
43 decomposition of organic matter under oxygen-limited conditions [3,6] —
44 has attracted particular attention. It yields biochar, a carbon-rich and
45 stable solid material that can be applied both as renewable fuel and as a
46 long-term carbon sequestration agent [7–10]. Biochar consists mainly of
47 aromatic carbon structures [11], and its properties are strongly dependent
48 on feedstock type — whether lignocellulosic (plant cell wall material made
49 of cellulose, hemicellulose and lignin [12]) or nutrient-rich — and on
50 pyrolysis parameters such as temperature, heating rate, and residence
51 time [9,13]. Its capacity of withstanding microbial breakdown results in
52 biochar surviving hundreds of years in soils, turning it into a long-term
53 carbon sequestering agent as well as an agent of minimizing climate
54 change [9,10].

55 Extensive research shows that higher pyrolysis temperatures decrease
56 volatile matter (VM) and increase fixed carbon (FC), leading to denser
57 aromatic structures and improved energy properties [7,11,14–16]. These
58 transformations are also associated with reduced combustion-related
59 emissions [16]. Proximate, ultimate, and calorimetric analyses remain the
60 standard tools for assessing such properties, as they provide data on
61 moisture (M), ash (A), volatile matter, fixed carbon, elemental composition
62 (C, H, N, S, O), and calorific values [10,17–20].

63 Feedstock type is equally decisive: lignocellulosic residues such as pine
64 cones, or hazelnut shells generally produce low-ash, carbon-rich biochars
65 with high heating values [8,21–26], whereas animal manures tend to yield
66 ash-rich chars with elevated N and S, limiting fuel performance but
67 enhancing agronomic potential [24–26]. In fact, Ippolito et al. [9]

68 demonstrate that wood-derived biochars are richer in carbon and poorer in
69 plant-available nutrients compared to manure-derived biochars, which
70 present opposite trends. Tomczyk et al. [27] corroborate these findings,
71 showing ash contents of $< 7\%$ for wood biochars versus $> 50\%$ for non-
72 wood (e.g., manure) biochars. Additionally, Mukome et al. [28] reveal that
73 feedstock type is a stronger predictor of ash content and C/N ratio than
74 other production variables.

75 Despite this broad knowledge base, comparative studies under uniform
76 pyrolysis conditions are still scarce. Regionally abundant resources such as
77 hazelnut shells, pine residues, oak pruning waste, and swine manure have
78 seldom been analysed side by side, which makes direct ranking for energy
79 vs. soil applications difficult. Another underexplored aspect is the role of
80 post-pyrolysis cooling, generally assumed to be inert (e.g., 'allowing the
81 reactor/sample to cool to room temperature under N_2 ') and treated as an
82 independent variable [29–31], although recent advances in process design
83 and thermal control suggests otherwise. Nebyvaev et al. [32] demonstrated
84 that slower post-torrefaction cooling significantly alters biochar's
85 composition, with higher ash, carbon and nitrogen contents, and lower H/C
86 and O/C ratios, indicating enhanced fuel properties. However, similar
87 effects have not yet been systematically investigated for biochar produced
88 through conventional pyrolysis, especially for feedstocks like hazelnut
89 shells or manure — a gap that this study aims to address.

90 Finally, calorific correlations (e.g., Channiwala-Parikh) are widely applied
91 to predict higher heating value (HHV) from elemental composition [33–35],
92 but deviations are reported for lignin-rich or highly aromatic chars,
93 stressing the need for experimental validation. Furthermore, current solid
94 biofuel standards (ISO 17225-2) are designed for wood pellets, not
95 biochars, which exposes a regulatory gap and complicates market uptake
96 [36].

97 Despite the abundance of general literature on biochar, the unique
98 compositional variability and high annual volume of Portugal's agro-
99 forestry residues—specifically pinecone, hazelnut shell, and local swine
100 manure—necessitates a dedicated, rigorous study. This work provides the
101 local and regional industrial data required by Portuguese circular economy
102 policies (e.g., the National Action Plan for Sustainable Bioeconomy [37]),

103 making the findings directly relevant for regional waste valorisation
104 strategies, a crucial aspect not addressed by generic international studies.
105 This study addresses these gaps by providing a comparative
106 thermochemical characterisation of five representative feedstocks from
107 northern Portugal (hazelnut shells, pine, pinecones, oak pruning residues,
108 and swine manure). By analysing proximate, ultimate, and calorimetric
109 properties under identical pyrolysis conditions, and by contrasting fast- and
110 slow-cooling regimes, this work clarifies how feedstock and post-treatment
111 affect biochar suitability for energy and agronomic applications. In
112 addition, empirical HHV predictions are validated against calorimetric
113 data, and results are benchmarked against ISO 17225-2 standards to
114 discuss the commercial implications of biochar valorisation. Specifically,
115 biochars, even those with superior calorific values, often diverge from the
116 premium standard's strict ash and nitrogen limits. This misalignment
117 necessitates experimental validation and benchmarking against the
118 standard to clearly define the market potential and regulatory barriers for
119 biochar valorisation. Crucially, the comparative results under uniform
120 conditions allow for a direct, unbiased ranking of intrinsic feedstock
121 properties, while the preliminary analysis of the slow-cooling sample
122 establishes a novel working hypothesis: that post-pyrolysis thermal history
123 is a non-inert, optimisable process lever for enhancing biochar quality.

124 **2. Methods and Materials**

125 **2.1. Feedstock and biochar production**

126 The northern region of Portugal generates significant and quantified
127 volumes of agricultural and forestry waste, making the selection of
128 feedstocks strategically critical for regional waste management. The
129 study's focus on these five materials is robustly justified by their high
130 annual availability in the NUTS II Norte region, a crucial factor for
131 industrial upscaling and circular economy goals. Official statistics for the
132 NUTS II Norte region confirm that the volume of pine and pine cone
133 residues exceeds 168,547 tonnes/year and oak residues total 65,376
134 tonnes/year [38]. Furthermore, the selected agricultural wastes are high-
135 volume: Dried manure is estimated at 38,456 tonnes/year [39,40], and the
136 significant availability of almond and hazelnut shells (totalling over 52,245

137 tonnes/year based on FAO/IPB data [41,42]) reinforces the strategic focus
138 on regional shell residues.

139 This study presents a detailed thermochemical characterization of biochars
140 produced from diverse biomass feedstocks subjected to controlled pyrolysis
141 conditions. The feedstocks used in this study were collected from two
142 primary sources. Woody samples, including hazelnut shells, pine,
143 pinecones, and oak pruning residues, were sourced from the Botanical
144 Garden of the University of Trás-os-Montes e Alto Douro (UTAD). The swine
145 manure was collected from UTAD's agricultural facilities.

146 **2.1.1. Pyrolysis Conditions**

147 All feedstocks were subjected to pyrolysis in a fixed-bed reactor at a final
148 temperature of 450°C. The heating conditions were standardized for all
149 runs to ensure direct comparability: a heating rate of 10°C/min was applied
150 until the peak temperature of 450°C was reached, followed by a holding
151 time of 60 min at the peak temperature. The 450°C final temperature was
152 selected as the standardized condition for this comparative study, as this
153 range is optimal for maximizing the fixed carbon content necessary for
154 solid fuel applications [5,7].

155 Crucially, the pyrolysis was conducted under ambient atmospheric air
156 (without external inert gas supply). The reactor was not purged, meaning
157 only the initial ambient air remained trapped inside the sealed vessel
158 before heating, establishing an oxygen-limited environment during the
159 process. This methodology, deviating from strict inert-gas pyrolysis, was
160 deliberately chosen to reflect simplified, non-purged industrial process
161 designs, focusing on ease of operation. While the temperature (450°C)
162 places the process firmly in the pyrolysis regime, the presence of air
163 introduces a controlled partial oxidation effect (similar to an intensified
164 torrefaction or mild oxidative pyrolysis). While this partial oxidation may
165 slightly reduce the final biochar yield compared to inert pyrolysis (due to
166 enhanced carbon combustion), it promotes a more aromatic, stable carbon
167 structure and a faster removal of oxygenated components, which enhances
168 the final fuel quality and is often desirable for solid fuel applications
169 [43,44].

170 **2.1.2. Post-Pyrolysis Cooling Procedures**

171 Following the 60 min holding time, two distinct cooling procedures were
172 employed to manage the highly reactive state of the hot biochar:

173 **a) Standard Rapid Cooling**

174 This procedure was applied to the five primary biochars (pine, pinecone, oak,
175 swine manure, and the standard hazelnut shell biochar). Upon completion of
176 the holding time, the reactor was immediately removed from the furnace and
177 tightly sealed to prevent fresh air ingress. The sealed reactor was then
178 rapidly cooled to near ambient temperature in a circulating water bath. This
179 immediate sealing and rapid cooling procedure is critical because the
180 biochar, still at 450°C upon removal, would otherwise rapidly undergo
181 uncontrolled auto-oxidation or combustion if exposed to a continuous supply
182 of atmospheric air, consuming carbon and altering the final product
183 properties. This procedure ensures the measured properties represent the
184 end-state of the 450°C pyrolysis stage.

185 **b) Case Study: Slow Cooling**

186 This procedure was performed as a single comparative experiment solely
187 using a hazelnut shell sample. Upon completion of the holding time, the
188 reactor containing the biochar was immediately sealed. The sealed reactor
189 was then left to cool passively inside the furnace until ambient temperature
190 was reached (approximately 48 hours). The sealing of the reactor was the
191 critical step to prevent fresh air ingress during the long cooling period.

192 The data for the slow-cooled hazelnut shell sample is included as a
193 preliminary finding based on a single experimental run, intended solely to
194 explore the potential impact of protracted post-pyrolysis conditions and
195 establish a novel working hypothesis. Further systematic experimentation
196 across all feedstocks is required to conclusively validate this effect.

197

198 **2.2. Proximate Analysis**

199 The proximate analysis determines the moisture, volatile matter, ash, and
200 fixed carbon contents of the samples, with all results expressed as weight
201 percentages.

202 Each biochar sample was placed in a Protherm PLF 100/6 furnace
203 (Protherm, Ankara, Turkey) at 105 °C until a constant weight was achieved,
204 indicating complete moisture removal in accordance to ISO 18134-3
205 standard [45]. The moisture content (%) was then determined from the
206 difference between the sample weight before and after drying.

207 From the dried samples obtained in the moisture analysis, a subsample was
208 weighed and placed in a sealed crucible. It was then heated at 900 °C until
209 its mass remained constant, indicating that all volatile organic components
210 had been released ISO 18123 [46] standard. The percentage of volatile
211 matter was calculated based on the mass loss during this stage. Following
212 the volatilisation step, the remaining residue was subjected to ashing in a
213 muffle furnace at 550 °C in accordance to ISO 18122 [47]. The process
214 continued until the sample reached a stable weight, confirming the
215 complete oxidation of the organic fraction. The ash content (%) was
216 subsequently determined from the weight difference before and after
217 ashing.

218 The fixed carbon content was then determined by subtracting the
219 percentages of moisture, volatile matter, and ash from the total mass
220 (100%) (Equation (1)).

$$\text{FC} = 100\% - \text{M}\% - \text{VM}\% - \text{A}\% \quad (1)$$

221 Each biochar sample was analyzed in triplicate, and the results are
222 expressed as the mean \pm standard deviation to ensure analytical
223 consistency.

224 **2.3. Ultimate Analysis**

225 Ultimate analysis was conducted to determine the elemental composition of
226 the biochar samples, specifically C, H, N, and S, in accordance with the ISO
227 16948 [48] standard. Samples were analysed using a ThermoScientific
228 FlashSmart CHNS/O elemental analyser (Waltham, MA, USA). The analyser
229 quantified C, H, N, and S contents directly, while O content was calculated
230 by subtracting the C, H, N, S, and ash contents from 100% (Equation (2)).

231 Each biochar sample was analyzed in triplicate, and the results are
 232 expressed as the mean \pm standard deviation to ensure analytical
 233 consistency.

$$\%O = 100\% - \%C - \%H - \%N - \%S - \%A \quad (2)$$

234 **2.4. Calorimetric Analysis**

235 The HHV and lower heating value (LHV) on an air-dry basis were
 236 determined using an isoperibolic calorimeter (Model 6300, Parr
 237 Instruments, Moline, IL, USA), in accordance with the procedures outlined
 238 in ISO 18125 [49]. Prior to analysis, the calorimeter was calibrated with a
 239 certified benzoic acid standard (Parr Benzoic Acid No. 3415, Moline,
 240 IL, USA) to verify and maintain the accuracy of the measurements.

241 Each biochar sample was analyzed in triplicate, and the results are
 242 expressed as the mean \pm standard deviation to ensure analytical
 243 consistency.

244 **2.5. Calculation of HHV**

245 Besides the calorimetric measurements, HHV of the biochars was also
 246 estimated with the correlation developed by Channiwala and Parikh [33].
 247 This approach uses the ultimate analysis to predict HHV and allows a
 248 direct comparison with the experimental results. The correlation is given
 249 by Equation (3).

$$\text{HHV (MJ/kg)} = 0.3491C + 1.1783H + 0.1034S - 0.1034O - 0.0151N - 0.0211A \quad (3)$$

250 where C , H , S , O , N and A represent the mass fractions (wt.%, dry basis) of
 251 carbon, hydrogen, sulphur, oxygen, nitrogen and ash, respectively.

252 **3. Results and Discussion**

253 The properties of the raw feedstocks (Table 1) serve as the baseline for
 254 evaluating the upgrading efficiency of the 450°C pyrolysis process. The
 255 lignocellulosic biomasses (pine, pinecone, hazelnut shell, oak) are
 256 characterized by high volatile matter (58-75%) and high oxygen content
 257 (>45%), typical of native biomass, resulting in relatively low HHV values
 258 (17.14-19.34 MJ/kg). **In contrast,** the pyrolysis process dramatically alters

259 this composition; the fixed carbon content, for instance, increases by a factor
 260 of up to 4 in the woody samples (Table 2), directly corresponding to the
 261 observed increase in the biochars' HHV (up to 32.20 MJ/kg) (Table 4). This
 262 fuel upgrading is directly reflected in the key biochar properties presented
 263 in subsequent tables: the substantial increase in Fixed Carbon (Proximate
 264 Analysis) and the dramatic reduction in O/C and H/C ratios (Ultimate
 265 Analysis) are the primary thermochemical indicators of enhanced Heating
 266 Value [50,51]. This comparison clearly demonstrates the significant fuel
 267 upgrading achieved by the thermal treatment, which is critical for their
 268 valorisation as solid fuels.

269

270 **Table 1.** Proximate, Ultimate Analysis, and HHV of Raw Feedstocks

Sample	Moisture _{ad} (wt%)	Volatile Matter _d (wt%)	Ash _d (wt%)	Fixed Carbon _d (wt%)	C _d (wt%)	H _d (wt%)	N _d (wt%)	O _d (wt%)	HHV _d (MJ/kg)
Pine	9.30±0.6 8	58.00±0.0 69	0.80±0.0 3	31.90±0.0 78	46.25±0.0 72	4.83±0.0 15	0.45±0.0 01	47.67±0.0 68	18.60±0.0 66
Pine cone	7.90±0.7 2	74.85±0.0 65	0.53±0.0 1	16.73±0.0 81	46.81±0.0 56	7.44±0.0 09	0.27±0.0 02	45.43±0.0 63	19.34±0.0 38
Hazelnuts shell	9.25±0.1 3	63.18±0.0 23	0.77±0.0 1	26.81±0.0 13	45.54±0.0 22	5.33±0.0 07	0.42±0.0 02	47.94±0.0 14	18.41±0.0 16
Swine manure	8.90±0.1 4	57.10±0.0 01	13.40±0.0 01	20.60±0.0 18	36.48±0.0 31	2.45±0.0 26	5.14±0.0 12	42.40±0.0 38	15.89±0.0 29
Oak prunings	11.20±0.0 14	62.00±0.0 03	1.80±0.0 1	25.00±0.0 12	46.14±0.0 44	4.95±0.0 15	0.82±0.0 02	46.30±0.0 23	17.14±0.0 11

271

ad - air dried basis; d - dry basis

272 When comparing the biochar compositions and properties with international
 273 literature, it is important to note the significant impact of geographical and
 274 climatic factors on feedstock characteristics. Factors such as soil type, local
 275 climate, harvesting practices, and wood species variants (provenance) mean
 276 that the initial composition of biomass (e.g., mineral content, moisture,
 277 lignin/cellulose ratio) can vary widely, as demonstrated by the comparison
 278 with, for example, Nordic feedstocks. Therefore, the use of Percent
 279 Difference serves primarily to confirm the fidelity of our thermochemical
 280 conversion process against established literature trends and expected
 281 compositional variance for different biomes, rather than implying perfect
 282 compositional matching with feedstocks from dissimilar biomes.

283 3.1. Proximate Analysis

284 Proximate analysis provides key indicators of fuel quality by quantifying
285 moisture, volatile matter, ash, and fixed carbon. Moisture content is
286 reported on an air-dried (ad) basis, representing the equilibrium moisture
287 of the biochar under typical laboratory storage conditions. Among the
288 samples, the slow-cooled hazelnut shell biochar presented the highest fixed
289 carbon (82.89%) and only 2.05% ash (Table 2), indicating good thermal
290 stability and low inorganic residue [21]. Such composition is typical of
291 lignocellulosic biochars produced at moderate pyrolysis temperatures,
292 reflecting extensive devolatilization and high carbon retention. The high
293 fixed carbon (>70%) and low volatile matter (<25%) contents observed in
294 all woody biochars are attributed to the 450 °C pyrolysis conditions, which
295 cause an almost complete decomposition of hemicellulose and cellulose.
296 The low VM content indicates efficient thermal treatment, resulting in a
297 highly effective devolatilization process that leaves a condensed, aromatic
298 carbon structure (fixed carbon), thereby enhancing the biochar's storage
299 stability and safety. Conversely, the high ash content in the swine manure
300 biochar (48.34%) is explained by the concentration of inorganic minerals
301 present in the feedstock, which are non-combustible and remain in the
302 solid residue after thermal treatment, effectively reducing the mass
303 fraction of the organic carbon component. The biochar derived from swine
304 manure exhibited the lowest fixed carbon content (36.12%) and the highest
305 ash content (48.34%) among all samples. Compared with the results
306 reported by Zhao et al. [22], for biochar produced at 500 °C (40.2% fixed
307 carbon, 48.4% ash, and 11.0% volatile matter), the fixed carbon content in
308 the present study is approximately 10% lower, whereas the ash content
309 shows a negligible difference of 0.1%.

310 The hazelnut shell biochar displayed a volatile matter content of 12.10%,
311 an ash content of 2.54%, and a fixed carbon level of 80.43%. When
312 compared to the reference data reported by Bartolucci et al.[3], which
313 reported at 450°C (20.38% volatile matter, 2.98% ash, and 76.64% fixed
314 carbon) some notable differences were observed. The Percent Difference
315 for volatile matter was 40.66%, indicating a significantly lower
316 devolatilization in the present sample. The ash content was 14.93% lower
317 than the reference, while the fixed carbon was 4.95% higher.

318 Differences in pyrolysis conditions, particularly temperature, heating rate
 319 and residence time, are probable causes for the observed deviations [22].
 320 Higher pyrolysis temperatures and longer residence times tend to reduce
 321 the volatile matter and ash content while increasing the fixed carbon
 322 fraction due to enhanced carbonization and aromatization processes [5,23].

323 **Table 2.** Biochar Proximate Analysis, Fuel Quality Ratios and Biochar Yield (All samples,
 324 except 'Slow-cooling hazelnut', were produced via Standard Rapid Cooling).

Sample	Moisture _{ad} (wt%)	Volatile Matter _d (wt%)	Ash _d (wt%)	Fixed Carbon _d (wt%)	Fuel Ratio (FC/VM)	Biochar Yield (wt%)
Pine	3.77 ± 0.02	20.75 ± 0.30	0.86 ± 0.01	74.61 ± 0.31	3.60	34.81 ± 0.72
Pinecone	6.49 ± 0.10	12.34 ± 0.18	0.96 ± 0.02	80.20 ± 0.21	6.50	36.05 ± 0.95
Hazelnut shell	4.94 ± 0.07	12.10 ± 0.05	2.54 ± 0.01	80.43 ± 0.12	6.65	32.74 ± 0.61
Swine manure	3.49 ± 0.03	12.06 ± 0.18	48.34 ± 0.18	36.12 ± 0.21	2.99	49.56 ± 1.22
Slow-cooling hazelnut shell	5.55 ± 0.09	9.51 ± 0.14	2.05 ± 0.03	82.89 ± 0.20	8.72	32.89 ± 0.58
Oak pruning residues	6.25 ± 0.02	19.49 ± 0.29	22.40 ± 0.35	51.86 ± 0.22	2.66	33.92 ± 0.84

325 ad - air dried basis; d - dry basis

326 The Volatile Matter (VM) content was drastically reduced (e.g., from near
 327 60% in woody biomasses to <25% in the biochar), which is a direct
 328 consequence of the near-complete devolatilization of hemicellulose and the
 329 majority of cellulose into volatile vapors and gases at this temperature.

330 In contrast, the FC content increased significantly across all woody
 331 biochars, reaching values >70%. For example, the hazelnut shell (rapid)
 332 saw its FC increase from near 27% in the raw biomass to near 82% in the
 333 biochar, representing an upgrading factor greater than 3. This increase
 334 results directly from the mechanism of carbonization and condensation of
 335 the solid residue, forming a more stable and dense aromatic carbon
 336 structure.

337 Ash content remained low (below 2%) in the woody biochars, confirming
 338 their high potential as a solid fuel. However, swine manure biochar stands
 339 out with an extremely high ash content (48.35%), which, coupled with its
 340 relatively high remaining VM (near 38%), confirms its unsuitability for
 341 direct energy applications due to the severe dilution of the organic fuel
 342 component by non-combustible inorganic minerals.

343 It is important to note that the ash content reported here represents the
 344 ash fraction concentrated in the biochar residue. The increase in ash
 345 percentage (wt%) from the feedstock (Table 1) to the biochar (Table 2) is a

346 standard thermochemical observation and a direct consequence of the loss
347 of organic material (volatile matter) during pyrolysis, which concentrates
348 the non-combustible inorganic components in the final solid product.

349 3.2. Ultimate Analysis

350 The ultimate analysis evaluates the elemental composition of biochars,
351 namely carbon, hydrogen, nitrogen, sulphur, and oxygen, which are critical
352 parameters for assessing their energetic potential and environmental
353 performance. Swine manure biochar contained the lowest concentrations
354 of carbon and oxygen (37.12% and 10.38%, respectively) and had the
355 highest concentrations of nitrogen and sulphur (2.52% and 0.09%,
356 respectively) among all samples analysed (Table 3). These results reflect
357 the typical composition of biochars derived from animal based residues,
358 which are generally rich in nutrients but have lower carbonization
359 efficiency [8,24]. The low carbon and high heteroatom contents may limit
360 its suitability for energy applications but mechanistically enhance its value
361 in agricultural use: the high ash content corresponds to a high
362 concentration of essential inorganic mineral nutrients (P, K, Ca, Mg) which
363 are concentrated in the solid phase after devolatilization, while the high N
364 content provides a slow-release nitrogen source [25]. Additionally, the high
365 nitrogen content may indicate a greater potential for pollutant emissions
366 such as nitrogen oxides during combustion processes, a factor that must be
367 considered in energy-related applications [26]

368 According to the literature, biochars derived from woody biomass such as
369 pine and pinecone are typically rich in carbon [5]. Consistent with this, the
370 biochars produced in this study exhibited high carbon content (80.96% and
371 82.26%, respectively), along with low nitrogen and oxygen levels. These
372 characteristics suggest a predominantly aromatic and thermally stable
373 carbon structure, favourable for carbon sequestration and energy-dense
374 applications [52-54]. In particular, the hydrogen content was higher in pine
375 (3.04%) than in pinecone (1.78%), potentially reflecting differences in the
376 degradation pathways of lignin and cellulose during pyrolysis [52,55].
377 When compared to data reported by Handiso, Pääkkönen, & Wilson [56] for
378 pine biochar at 450°C (82.28% carbon, 3.42% hydrogen, 12.65% oxygen,
379 and 0.08% nitrogen) the results obtained in this study show a good overall
380 agreement. The carbon content of pine differed by only 1.6% (Percent

381 Difference), while hydrogen content was 11.1% lower, and oxygen showed
382 a 10.5% variation.

383 A deviation in nitrogen content was observed, with a relative difference of
384 92.6%, however, the absolute nitrogen levels remained low in both cases,
385 minimizing its impact on performance considerations.

386 Among all samples analysed, the slow-cooling hazelnut shell biochar
387 exhibited the highest carbon content (82.97%), indicating a high degree of
388 carbonization and structural condensation [53]. In contrast, hazelnut shell
389 biochar removed immediately after pyrolysis showed a slightly lower
390 carbon value (76.88%) and higher oxygen level (17.33%), emphasizing the
391 influence of post-pyrolysis cooling conditions in determining final elemental
392 composition [57]. Compared with the values reported by Bartolucci et al.
393 [3] (80.44% carbon, 2.59% hydrogen, 13.77% oxygen and 0.21% nitrogen)
394 hazelnut shell sample cooled inside the reactor demonstrated strong
395 agreement in carbon content, with a Percent Difference of only 3.1%. The
396 hydrogen content in this study (1.78%) was 31.3% lower, while the oxygen
397 content (12.26%) was 11.0% lower. Nitrogen content (0.94%) showed the
398 largest deviation, with a relative difference of 347.6%. Despite this, the
399 absolute nitrogen levels remained low in both cases.

400 **Table 3.** Ultimate Biochar Analysis

Sample	N _d (wt%)	C _d (wt%)	H _d (wt%)	S _d (wt%)	O _d (wt%)
Pine	1.16 ± 0.02	80.96 ± 0.49	3.04 ± 0.05	n.d.	13.97 ± 0.48
	0.97 ± 0.01	82.26 ± 0.96	1.78 ± 0.06		n.d.
Pinecone	0.99 ± 0.02	76.88 ± 1.68	2.27 ± 0.07	n.d.	17.33 ± 1.75
	2.52 ± 0.04	37.12 ± 0.29	1.54 ± 0.04		0.09 ± 0.01
Swine manure	0.94 ± 0.02	82.97 ± 1.67	1.78 ± 0.01	n.d.	12.26 ± 1.65
	2.02 ± 0.05	52.39 ± 1.20	1.21 ± 0.05		n.d.
Slow-cooling hazelnut shell					
Oak pruning residues					

401 d - dry basis; n.d. - Not detected

402 Woody biomass biochars (pine and pinecone) also showed high carbon
403 content (80.96% and 82.26%, respectively) and low nitrogen and oxygen
404 levels, suggesting a stable, aromatic carbon structure favourable for
405 energy applications.

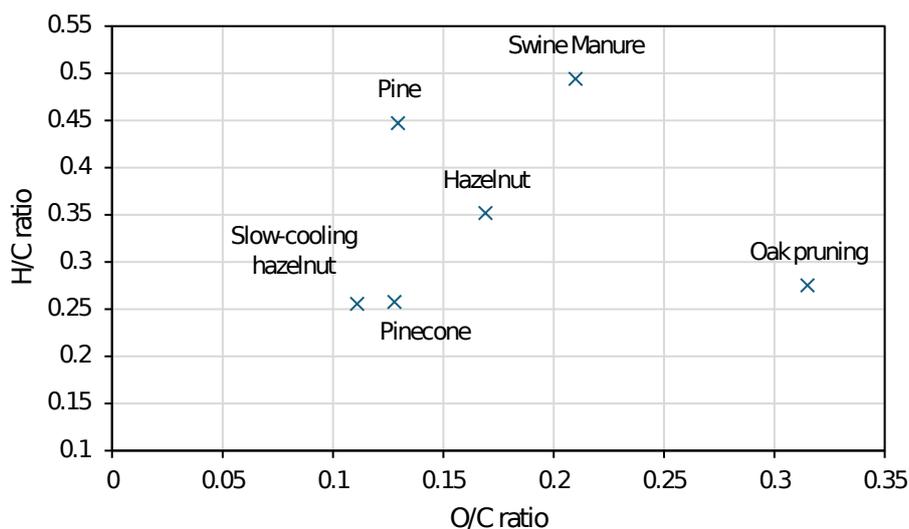
406 **3.3. The Effect of Cooling Rate: A Promising Preliminary Finding**

407 One of the most notable outcomes of this study is the influence of post-
408 pyrolysis conditions. The slow-cooled hazelnut shell sample showed a
409 considerable increase in fixed carbon content (from 80.43% to 82.89%) and
410 total carbon (from 76.88% to 82.97%).

411 The observed enhancement in Fixed Carbon and reduction in O/C and H/C
412 (visually confirmed in Figure 1) suggests that the cooling phase is not
413 chemically inert. This is supported by mechanistic understanding: the
414 prolonged residence time of nascent pyrolysis vapors (tars) at elevated
415 temperatures within the sealed reactor promotes their secondary
416 decomposition and condensation (secondary aromatization) onto the solid
417 char surface. This process effectively drives the further removal of residual
418 oxygen and hydrogen, leading to the observed increase in carbonization
419 and fuel quality. While these observations are limited to one feedstock and
420 represent a preliminary finding, it strongly suggests that the cooling phase
421 is not chemically inert and may allow for secondary aromatization
422 reactions. This is likely due to the prolonged residence time of nascent
423 pyrolysis vapors (tars) at elevated temperatures within the sealed reactor,
424 promoting their secondary decomposition and condensation (secondary
425 aromatization) onto the biochar surface. This mechanism effectively
426 increases the yield of fixed carbon and drives the further loss of
427 oxygenated functional groups, as visually confirmed by the shift in the Van
428 Krevelen diagram. This constitutes a promising research avenue for
429 optimizing biochar quality, which should be explored in future work.

430 **3.4. Van Krevelen Diagram and Degree of Carbonization**

431 The Van Krevelen diagram (Figure 1) visually represents the degree of
432 carbonization for each biochar. The woody biomass biochars (pine,
433 pinecone, hazelnut shell) cluster together, characterized by low H/C (<0.5)
434 and O/C (<0.15) ratios, indicating a high degree of coalification [58]. The
435 swine manure biochar is clearly separated, showing a less carbonized
436 nature. Crucially, the slow-cooled hazelnut shell sample is shifted further
437 towards the origin (lower H/C and O/C) compared to its fast-cooled
438 counterpart, visually confirming the enhanced carbonization effect of the
439 slower cooling process.



440

441 **Figure 1.** Van Krevelen diagram (H/C vs. O/C atomic ratios) for the produced biochars.442 **3.5. Calorimetric Properties and Higher Heating Value Validation**

443 Calorimetric analysis determines the higher and lower heating values,
 444 providing a direct measure of the energy potential of biochars. Among the
 445 tested samples, hazelnut shell biochar exhibited the highest energy
 446 content, with a HHV value of 32.20 MJ/kg and a LHV of 31.64 MJ/kg,
 447 followed closely by pine and pinecone with LHV of 29.82 MJ/kg and 29.29
 448 MJ/kg, respectively (Table 4). In contrast, the swine manure biochar
 449 showed significantly lower values, with a LHV of 12.05 MJ/kg, reflecting its
 450 higher ash and lower fixed carbon contents. However, minor discrepancies
 451 are observed, particularly for the hazelnut shell biochar, where the
 452 measured HHV (32.20 MJ/kg) is significantly higher than the predicted
 453 value (27.65 MJ/kg), representing a Percent Difference of 16.46%.

454 Compared to literature data, the LHV of hazelnut shell biochar obtained in
 455 this study (31.64 MJ/kg) was slightly higher than the 28.73 MJ/kg reported
 456 by Bartolucci et al. [3], corresponding to a relative difference of
 457 approximately 10.15%. Despite this variation, both results indicate a high
 458 energy density, aligning with the elevated carbon content observed in this
 459 type of biomass [53]. The pinecone biochar LHV (29.29 MJ/kg) reflects
 460 typical woody biomass characteristics, with high carbon and low ash and
 461 moisture contents. Wu et al. [59] reported a LHV of 28.92 MJ/kg, the
 462 relative difference between both values is approximately 1.29%,

463 underscoring the consistency of the results and confirming pinecones as a
 464 reliable high-energy feedstock for thermochemical applications.

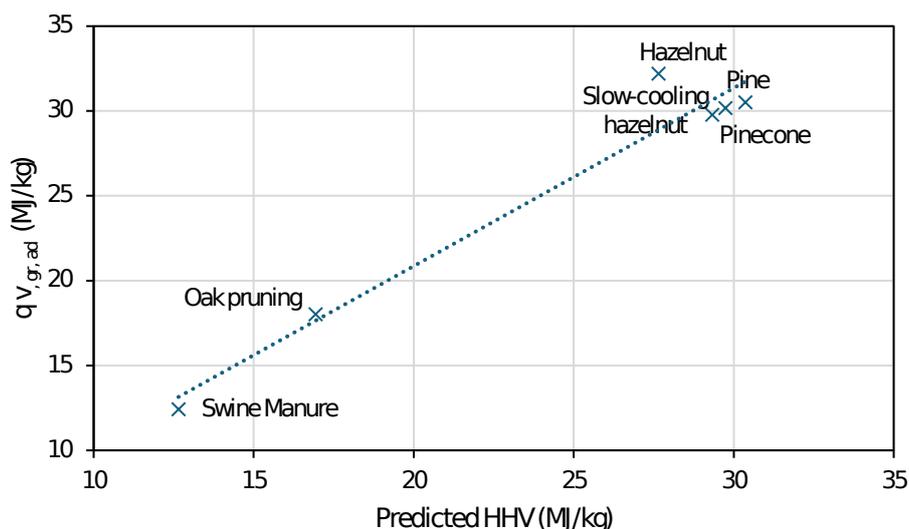
465 **Table 4.** Calorimetric Analysis of biochar

Sample	HHV _{ad} (MJ/kg)	LHV _{ad} (MJ/kg)	Predicted HHV (MJ/kg)
Pine	30.51 ± 0.79	29.82 ± 0.79	30.37
Pinecone	29.78 ± 0.12	29.29 ± 0.12	29.33
Hazelnut shell	32.20 ± 0.26	31.64 ± 0.26	27.65
Swine manure	12.44 ± 0.08	12.05 ± 0.08	12.65
Slow-cooling hazelnut shell	30.17 ± 0.06	29.70 ± 0.06	29.74
Oak pruning residues	18.03 ± 0.09	17.65 ± 0.09	16.94

466 ad - air dried basis

467 To validate the consistency of the analytical data, the HHV was predicted
 468 using the Channiwala and Parikh empirical [33] equation and compared
 469 against the measured values (Table 4). The strong correlation between the
 470 predicted and measured values confirms the high quality and reliability of
 471 the proximate and ultimate analyses performed.

472 The comparison between the measured HHV values and those predicted by
 473 the Channiwala and Parikh [33] empirical equation (Table 4) demonstrates
 474 a strong overall correlation, which validates the accuracy of the proximate
 475 and elemental analyses performed. As visually represented in Figure 2,
 476 there is a strong linear correlation between the two sets of values, with
 477 most data points clustering closely around the ideal 1:1 correlation line.
 478 However, minor discrepancies are observed, particularly for the hazelnut
 479 shell biochar, where the measured HHV (32.20 MJ/kg) is significantly
 480 higher than the predicted value (27.65 MJ/kg).



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Figure 2. Correlation between the measured HHV of biochar samples and the HHV values predicted by the Channiwala and Parikh empirical equation. The dashed line represents the ideal 1:1 correlation.

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These differences can be attributed to several factors. Firstly, empirical equations like the Channiwala and Parikh model are developed based on a large dataset of various feedstocks, and while they are highly reliable for general applications, they may not perfectly capture the unique chemical structure and complex interactions of specific biomass types [34]. The high lignin content and subsequent aromatic structure of woody biochars, such as that from hazelnut shells, can lead to a higher energy density [35] than predicted by simple elemental correlations.

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Secondly, the equation's reliance on elemental composition alone may not fully account for the complex char-forming reactions and post-pyrolysis changes [60]. As demonstrated by our finding on the slow-cooled hazelnut shell sample, the final properties of biochar are not only a function of the peak pyrolysis temperature but also of conditions during the cooling phase. This suggests that the measured HHV reflects a more complete thermochemical profile than can be predicted by a formula based solely on the final elemental percentages.

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Despite these minor variations, the strong linear correlation observed across all samples confirms the high quality of our experimental data and supports the use of proximate and elemental analyses as a reliable method for the thermochemical evaluation of biochars.

505 **3.6. Correlation between Feedstock Composition and Biochar** 506 **Properties**

507 The superiority of woody-derived biochars (hazelnut shell, pinecone) in
508 terms of fixed carbon (up to 82.89%) and lower heating value (up to 31.64
509 MJ/kg) is directly attributed to their lignocellulosic composition. Lignin, in
510 particular, is known to produce a more aromatic and thermally stable
511 biochar structure during pyrolysis. This is in contrast with swine manure,
512 which is richer in nutrients and inorganic matter, resulting in a much
513 higher ash content (48.34%). Literature confirms that the high thermal
514 resistance of lignin contributes to greater biochar yield and fixed carbon
515 content compared to cellulose and hemicellulose [12].

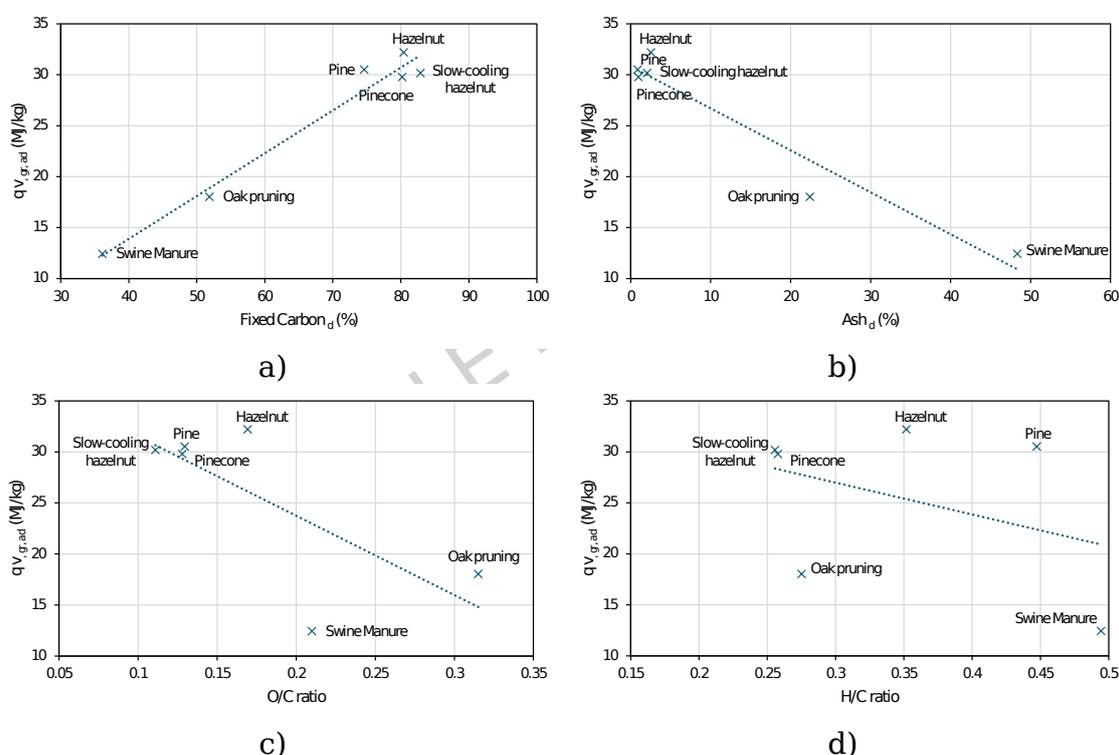
516 **3.7. Fuel Ratios and Combustion Behaviour**

517 The Fuel Ratio fixed carbon/Volatile Matter (FC/VM) is a key indicator of
518 combustion quality [61]. As shown in Table 2, the slow-cooled hazelnut
519 shell and pinecone biochars exhibit the highest ratios, indicating a slower,
520 more stable combustion characteristic of high-quality solid fuels [62]. The
521 swine manure biochar has a significantly lower ratio, reinforcing its lower
522 suitability for combustion applications. Although the Oak pruning's sample
523 exhibited the lowest Fuel Ratio (≈ 3.0) in the woody set, the most
524 significant functional result remains the swine manure biochar, whose low
525 ratio is compounded by the 48.35% Ash content, making it the
526 overwhelming outlier for fuel applications.

527 **3.8. Graphical Correlation Analysis**

528 To deepen the understanding of the relationships between the biochar
529 properties, several graphical correlations were prepared (Figure 3). Figure
530 3a reveals a strong positive and linear correlation between the HHV and
531 the fixed carbon content, with a determination coefficient (R^2) close to 1.
532 This relationship demonstrates that a higher degree of carbonization
533 directly results in a fuel with greater energy density [63]. In contrast,
534 Figure 3b shows a clear negative correlation between HHV and Ash
535 content, illustrating how the presence of incombustible inorganic matter
536 dilutes the fuel's energy content [64]. The swine manure biochar is an
537 outlier in these graphs, reinforcing its distinct composition.

538 Figure 3c shows a negative correlation between HHV and the O/C atomic
 539 ratio, indicating that the removal of oxygen during pyrolysis is essential for
 540 increasing the calorific value [65]. The decrease in the H/C ratio (Figure
 541 3d) reflects the loss of hydrogen and the increase in the aromaticity and
 542 stability of the carbon structure [66]. Biochars with low H/C ratios, such as
 543 those from pine (H/C = 0.45) and pinecone (H/C = 0.26), and especially the
 544 slow-cooled hazelnut shell sample (H/C = 0.26), show the highest HHV
 545 values. This phenomenon is aligned with the carbonization process, where
 546 the formation of a more condensed and stable carbon matrix (less
 547 hydrogen) increases the calorific value [67]. Therefore, this correlation
 548 reinforces the robustness of pyrolysis as a process to create high-energy-
 549 density solid fuels from biomass [15].



550 **Figure 3.** Correlations between biochar properties. (a) HHV vs. fixed carbon; (b) HHV vs.
 551 Ash Content; (c) HHV vs. O/C atomic ratio; (d) HHV vs. H/C atomic ratio.

552 These correlations not only validate the analytical data but also provide a
 553 comprehensive view of the thermochemical conversion mechanisms of
 554 biomass and the interrelationships between the biochar properties.
 555 Figure 3d further supports the trends observed in the previous correlations
 556 by illustrating a clear, strong negative relationship between the HHV and
 557 the H/C atomic ratio. This correlation is a direct consequence of the
 558 pyrolysis process itself. As biomass is heated, deoxygenation and

559 dehydrogenation reactions occur, progressively breaking down the original
560 lignocellulosic structure [12]. This process leads to the loss of hydrogen
561 and oxygen in the form of water, methane, and other gases, leaving behind
562 a more condensed and stable carbon matrix [67]. Consequently, a lower
563 H/C ratio signifies a higher degree of carbonization and aromaticity, which
564 are the primary drivers of increased energy density [68]. This is evident as
565 the highest HHV values, for instance, the slow-cooled hazelnut shell
566 sample, correspond to the lowest H/C ratios. The positioning of the swine
567 manure biochar as an outlier on this graph, with a significantly higher H/C
568 ratio than the woody biochars, reinforces its distinct chemical composition
569 and the lack of extensive carbonization during pyrolysis due to its high
570 inorganic content [27]. This finding directly complements the insights
571 gained from the Van Krevelen diagram (Figure 1), where the biochar
572 samples migrate towards the origin as they become more carbonized. Both
573 graphical representations collectively validate the effectiveness of pyrolysis
574 as a tool for increasing the energy density of biomass and confirm that the
575 final properties of the biochar are directly linked to its degree of
576 aromatization and condensation.

577 In conclusion, while the strong linear correlations observed between and
578 compositional parameters (fixed carbon, H/C, O/C ratios) align with
579 established literature for biochar production at (even under partial
580 oxidation conditions), the utility of this analysis lies in highlighting the
581 novel deviations observed in the dataset. Firstly, the swine manure biochar
582 acts as a distinct outlier, significantly lowering the overall correlation and
583 demonstrating its fundamental unsuitability as a standalone solid fuel due
584 to high ash content, regardless of the fixed carbon value. Secondly, and
585 crucially, the Slow-Cooled hazelnut shell sample exhibits a distinct
586 displacement relative to the main rapid-cooled group. Specifically, when
587 plotted on the Van Krevelen diagram or against fixed carbon, this sample
588 demonstrates the lowest H/C and O/C ratios and highest fixed carbon
589 content for the given pyrolysis temperature. This superior fuel quality,
590 achieved solely by modifying the post-pyrolysis cooling rate (i.e., time
591 under sealed conditions), provides concrete graphical evidence that the
592 thermal history after the peak temperature is a critical, chemically active
593 process, strongly supporting the major outcome claimed in this study. The
594 strong correlations observed in Figure 3, while confirming established

595 biochar trends, serve two crucial functions for this comparative study.
 596 Firstly, they validate the analytical quality and the fidelity of the conversion
 597 process across five diverse feedstocks. Secondly, the linear relationship
 598 between HHV and Fixed Carbon ($R^2 \approx 1$) provides the quantitative basis for
 599 the proposed Hierarchical Valorisation Model, visually confirming that the
 600 degree of carbonization is the primary intrinsic driver of the fuel's energy
 601 potential hierarchy for these feedstocks.

602 3.9. Stoichiometric Air Requirement

603 The stoichiometric (theoretical) air required for complete combustion is a
 604 fundamental parameter for boiler design [69]. Fuels with a higher degree
 605 of carbonization, such as the slow-cooled hazelnut shell, require more air
 606 per kg of fuel (Table 5). Conversely, fuels with high oxygen content, like the
 607 oak pruning residue biochar, require less external air for combustion.
 608 Given the significant differences in ash content, a detailed analysis of the
 609 mineral composition is essential for evaluating combustion risks. While
 610 specific XRF data are reserved for future work, the nature of the feedstocks
 611 allows for predictive inferences. The high ash content in swine manure is
 612 anticipated to be rich in alkaline earth metals (Ca, Mg) and nutrients (P, K),
 613 increasing the risk of slagging and fouling at typical combustion
 614 temperatures. Conversely, the woody biochars are expected to have ash
 615 predominantly composed of Ca and K, which contributes less to severe
 616 slagging but influences ash melting behaviour.

617 **Table 5.** Calculated Stoichiometric Air Requirement

Sample	$O_{2,sto}$ (kg O_2 / kg fuel)	Stoichiometric Air (kg air / kg fuel)
Pine	2.26	9.75
Pinecone	2.20	9.47
Hazelnut shell	2.06	8.87
Swine manure	1.01	4.36
Slow-cooling hazelnut shell	2.23	9.62
Oak pruning residues	1.27	5.49

618 **3.10. Cooling Kinetics as a Lever for Energy-Efficient Biochar** 619 **Optimization**

620 While numerous studies correlate biochar properties with peak pyrolysis
621 temperature, our work introduces a novel dimension by investigating post-
622 pyrolysis thermal history. The finding that the slow-cooled hazelnut shell
623 sample exhibits the lowest O/C and highest HHV (for the 450°C group)
624 demonstrates that the cooling phase is not chemically inert. This suggests
625 that extended thermal exposure post-pyrolysis promotes greater C and H
626 condensation and removal of residual oxygenated compounds, offering a
627 new lever for process optimization that minimizes energy consumption
628 associated with excessively high peak temperatures. This observation
629 opens the door for further process modelling to integrate cooling dynamics
630 into biochar quality prediction frameworks.

631 **4. Strategic Implications and Future Outlook**

632 This study provided an in-depth thermochemical characterization of
633 biochars from locally sourced biomass in northern Portugal. Woody
634 biomass-derived biochars consistently showed superior fuel properties
635 compared to swine manure biochar. Beyond laboratory-scale
636 characterization, these findings carry practical relevance for regional
637 biomass management.

638 **4.1. A Hierarchical Valorisation Model for the Region**

639 Based on the comprehensive thermochemical characterization of the
640 biochars, a hierarchical waste management model is proposed for Northern
641 Portugal. This model aims to maximize the value and impact of each
642 feedstock, classifying biochars into three distinct application levels, each
643 justified by the experimental data obtained.

644 **Level 1: High-Quality Energy Valorisation (Premium Biochars)**

645 This level includes biochars from hazelnut shell and pinecone. Their
646 classification is due to their exceptional fuel properties: low ash content
647 (2.54% and 0.96%, respectively), high fixed carbon (>80%), and a very high
648 LHV, reaching 31.64 MJ/kg for hazelnut shell and 29.29 MJ/kg for
649 pinecone. These values far exceed the ISO 17225-2 standard for premium
650 wood pellets (≥ 16.5 MJ/kg) [36]. These biochars are ideal for replacing

651 fossil fuels in industrial systems and for producing high-energy-density
652 pellets [70]. The slow-cooled hazelnut shell sample, in particular, with an
653 LHV of 29.70 MJ/kg and the highest fixed carbon content (82.89%),
654 represents an even higher niche product.

655 **Level 2: General Energy Valorisation or Blending**

656 Biochars from pine and oak pruning residues fall into this category.
657 Although they show good energy potential, their ash contents are higher
658 (0.86% for pine and 22.40% for oak pruning residues) than those of
659 premium biochars. The oak pruning biochar, in particular, has an ash
660 content that makes it unsuitable for standard combustion systems, but it
661 still maintains a LHV of 17.65 MJ/kg. These materials are more suitable for
662 combustion systems with a higher tolerance for ash, or they can be used in
663 blends (co-combustion) to improve the energy quality of other lower-value
664 solid fuels, such as the swine manure biochar itself or raw biomass
665 residues [71].

666 **Level 3: Nutrient Recycling and Soil Improvement**

667 The swine manure biochar is classified at this valorisation level. Its
668 unsuitability as a standalone fuel is evident from its LHV of 12.05 MJ/kg
669 and, crucially, its extremely high ash content of 48.34%. However, this
670 energetic "disadvantage" is its greatest agricultural advantage, as the ash
671 is rich in essential minerals such as phosphorus and potassium, and the
672 biochar itself has a significant nitrogen content (2.52%) [72]. This makes it
673 an excellent soil amendment and slow-release fertilizer, contributing to
674 sustainable agriculture and the circular economy of the region. Its
675 application to the soil not only recycles nutrients but also acts as a carbon
676 sequestration agent, demonstrating its superior environmental value [73].

677 In conclusion, the proposed hierarchical valorisation model offers a
678 strategic framework for managing Northern Portugal's diverse agro-
679 forestry residues. This approach moves beyond a 'one-size-fits-all' view of
680 biochar by recognizing that its optimal use depends fundamentally on the
681 feedstock's inherent properties. By scientifically classifying these biochars,
682 this model not only promotes the most efficient use of each resource (from
683 premium fuel production to nutrient-rich soil amendment) but also
684 maximizes both the economic value and the environmental benefits of

685 biomass valorisation. This tiered strategy provides a clear and actionable
 686 pathway for regional stakeholders to contribute to a more sustainable,
 687 circular economy, reducing waste while generating valuable products and
 688 mitigating climate change [74].

689 **4.2. Carbon Sequestration Potential**

690 The low H/C (<0.5) and O/C (<0.15) atomic ratios for the woody biochars
 691 indicate a high degree of carbonization and increased aromaticity.
 692 Aromatic structures are significantly more resistant to microbial
 693 decomposition, ensuring that the sequestered carbon remains stable in soil
 694 for hundreds of years, unlike the original biomass [75]. This quantifies the
 695 long-term climate benefit of converting these residues into biochar,
 696 creating a stable carbon reservoir [73].

697 **4.3. Comparison with ISO 17225-2 Solid Biofuel Standards**

698 From a commercial perspective, comparing the best-performing biochars to
 699 the ISO 17225-2 standard for premium wood pellets (Class A1) provides a
 700 useful benchmark (Table 6) [36]. The outstanding calorific values of
 701 hazelnut shell (31.64 MJ/kg) and pinecone biochars (29.29 MJ/kg) place
 702 them well above the minimum threshold of 16.5 MJ/kg, confirming their
 703 competitiveness as high-energy solid fuels. However, other parameters
 704 such as ash (2.54% for hazelnut shell) and nitrogen content (~1% for both
 705 woody biochars) exceed the strict limits set for premium-grade pellets.

706 **Table 6.** Comparison of Top Biochars with ISO 17225-2 (Class A1) Standard [36]

Parameter	Hazelnut shell Biochar	Pinecone Biochar	ISO 17225-2 (Class A1 - Premium Wood Pellets)
LHV (MJ/kg, ad)	31.64	29.29	≥ 16.5
Ash Content (% _d)	2.54	0.96	≤ 0.7
Nitrogen Content (% _d)	0.99	0.97	≤ 0.3
Sulphur Content (% _d)	n.d.	n.d.	≤ 0.04

707 n.d. - Not detected

708 This divergence highlights that while the biochars significantly exceed the
 709 calorific value requirements, their ash (for hazelnut shell) and nitrogen
 710 contents are higher than the premium class standard. This leads to a rich
 711 discussion: biochar is a fantastic fuel, but to be commercialized as a high-

712 quality standard product, it might require post-treatment, blending with
713 other materials, or the development of new, biochar-specific standards to
714 account for its unique properties. The data highlights a critical gap
715 between existing solid biofuel standards and the characteristics of high-
716 quality biochars, suggesting a need for industry-specific guidelines.

717 **4.4. Operational Implications of Ash and Nitrogen Content**

718 The high ash contents in swine manure (48.34%) and oak pruning waste
719 (22.40%) are strong indicators of potential operational problems in boilers,
720 such as slagging and fouling [76]. Manure-derived ash is typically rich in
721 potassium (K), phosphorus (P), and silicon (Si) [77]. These elements are
722 known to lower the ash melting point, leading to slag formation and
723 deposition on heat exchange surfaces [78]. This increases maintenance
724 costs and reduces thermal efficiency, providing a strong argument against
725 using these feedstocks as pure fuels [76]. This is supported by studies
726 noting the high concentration of problematic ash-forming elements in
727 manure-derived biochar [23].

728 **5. Conclusions**

729 In summary, this study provides a high-quality comparative
730 thermochemical characterization of regionally significant Portuguese agro-
731 forestry residues, establishing the woody biochars (pine, hazelnut shell,
732 pinecones) as highly efficient solid fuels with HHV values exceeding 30
733 MJ/kg. The most notable finding of this comparative analysis is the
734 unsuitability of swine manure for energy valorisation due to its extremely
735 high ash and nitrogen content. Furthermore, the preliminary results from
736 the slow-cooled hazelnut shell sample showed a considerable increase in
737 fixed carbon content (from 80.43% to 82.89%) and total carbon (from
738 76.88% to 82.97%). The observed enhancement in fuel quality via slow-
739 cooling suggests a promising avenue for biochar optimization. However, it
740 must be acknowledged that extending the processing time carries an
741 implicit energetic penalty. For this optimization to be industrially viable,
742 the thermal energy retained in the reactor during the prolonged cooling
743 phase must be effectively recovered or integrated into the overall process
744 heat balance, particularly in large-scale pyrolysis units. A dedicated techno-

745 economic or LCA study would be necessary to quantify the net energy gain
746 and carbon emissions impact of implementing slow-cooling commercially.

747 Woody biomass-derived biochars, such as hazelnut shell and pinecone,
748 exhibited uniformly low volatile matter, high fixed carbon, and high
749 calorific values profiles agreeing with the literature. In contrast, swine
750 manure-derived biochar displayed higher ash content, lower fixed carbon,
751 and significantly reduced calorific value, corroborating the prior
752 publications on animal waste residues, which often yield biochars with
753 lower energy density and higher inorganic content.

754 The anticipated pattern of lower volatile content and higher fixed carbon
755 levels in more carbonized biochars was clearly observed. These shifts are
756 critical for biochar's utility as a renewable solid fuel: higher fixed carbon
757 and lower ash result in greater heat release upon combustion, reduced
758 environmental emissions, and improved thermal stability, making woody
759 biochars more suitable for energy generation.

760 By combining these experimental observations with literature benchmarks,
761 this work identifies hazelnut shell and pine-derived biochars as the most
762 promising feedstocks for solid fuel applications in the regional context.
763 Meanwhile, manure-derived biochar shows greater value as a nutrient
764 source or soil amendment, though with limited energy potential.

765 Considering all results, the study supports the dual role of biochar, as both
766 a tool for carbon sequestration and a viable solid biofuel alternative,
767 especially when produced from agroforestry residues. It highlights the
768 importance of feedstock selection and pyrolysis conditions in optimizing
769 biochar quality. These findings contribute to sustainable biomass
770 management strategies in Portugal and offer guidance for integrating
771 biochar into renewable energy systems and carbon mitigation pathways.

772 While the results underscore the promise of lignocellulosic residues for
773 energy applications, future work should explore the impact of process
774 scale-up and the integration of catalytic or post-treatment strategies to
775 further enhance biochar performance. Crucially, the full assessment of
776 biochar as a solid fuel requires detailed combustion and emission analysis
777 (e.g., thermal efficiency, NO_x, and SO_x emissions), which is the primary
778 limitation of the current study and a critical next step. Moreover, future

779 work will focus on Level 2 mechanistic analysis, including spectroscopic
780 characterization and thermodynamic process modeling.

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785 **Data Availability Statement:** The raw data supporting the conclusions of this
786 article will be made available by the authors on request.

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