



Methods and Composites for Surfactant Removal From Wastewater: A Review

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Abstract The COVID-19 pandemic has exacerbated water quality issues due to the use of substances such as soaps, detergents, and hand sanitizers, which contain surfactants as their key ingredient. These products are modified to enhance their properties, thereby increasing their hazardous chemical impact on the environment, necessitating efficient remediation materials and methods. Surfactants are also released into the environment from various industrial processes. Compared to other surfactant removal techniques, adsorption offers several advantages, including ease of design, simplicity of use in the technical realm, and adaptability to various treatment formats. Adsorption operates across a wide pH range and in several environments. Adsorption is efficient, profitable, requires minimal energy, and has no harmful byproducts. Adsorbents can be developed using various biomass products, nanomaterials, polymeric materials, zeolites, and clays. Composites represent a much efficient alternative material for the elimination of surfactants. A composite of bentonite, sodium bisulfite, polyacrylamide, and aluminum sulphate confirmed a reduction in the surfactant concentration by 82 %, and Chemical Oxygen Demand (COD) by 65 % from a textile wastewater sample. Composite

adsorbents made of zeolite and eggshells effectively removed surfactants from samples. The final adsorbent revealed 88% COD removal rate. The presented manuscript analyses the conventional methods for surfactant removal, especially focusing on composites as adsorbents. Future perspectives have been emphasized for the use of composites, and the performance of various composites for surfactant removal has been discussed at length.

Keywords Composites · Surfactants · Wastewater Treatment · Adsorption · Adsorbents

1 Introduction

Water scarcity is a pressing issue, with only 2.99% of available water being fresh or accessible for drinking. Population growth, urban progress, pollution, and climate change contribute to this shortage. United Nations International Children's Emergency Fund (UNICEF) reports that 750 million people globally lack access to fresh water, and the World Water Council (WWC) predicts that 3.9 billion people will live in water-deficient regions by 2030. Initiatives like wastewater purification using sustainable techniques and materials are being implemented to address water scarcity issues. This ensures availability and sustainable management of surface water as per the requirement of Sustainable Development Goals (SDGs-6) of the United Nations (Obaideen et al., 2022). The

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adsorption technique with various adsorbents for water remediation is one such aspect of water purification (Jaspal et al., 2023). Figure 1 depicts adsorption as a process aligned with United Nations Sustainable Development Goal 6. Wastewater streams from domestic and industrial activities contain organic compounds known as emerging contaminants (ECs), which comprise of insecticides, medications, hormones, plasticizers, food additives, wood preservatives, detergents, surfactants, decontaminators, flame retardants, and other organic compounds. These contaminants are not subject to regular restrictions and can be fatal to aquatic and human life. Cost-effective tertiary treatment techniques are required since conventional primary and secondary water treatment facilities find it challenging to remove these harmful contaminants effectively. Owing to its affordable initial cost, high efficiency, and simple working model, adsorption is a viable technique for removing EC. According to research, EC is removed from water and wastewater using a variety of adsorbents, such as activated carbons, modified biochar, nano adsorbents, and composite adsorbents (Sophia and Lima, 2018).

Reclamation of wastewater is a sustainable approach to water scarcity; nevertheless, water contains significant amounts of detergents, including surfactants, which are hazardous to the environment and human health. Since surfactants impede the activity of microorganisms, biological remedies are inefficient. Options for chemical therapy can be expensive and affect the general consensus. Better adsorbents for treating and eliminating surfactants have been found in low-priced sustainable materials such as silica gel, zeolite minerals, activated carbon, biomasses such as mussel shells, rubber tyre granules, fly ash and powdered coarse blast furnace slag (James & Ifealebuegu, 2018).

Adsorption is an established technique that uses various materials to remove numerous contaminants, including organic pollutants. Metal oxides and their composites can be used for the adsorptive removal and photocatalytic degradation of organic pollutants comprising dyes, insecticides, fertilizers, pharmaceutical components, organohalides, phenols, surfactants, and even nutrients. The highly selective properties of nanostructured metal oxides and their composites, including their specific crystalline

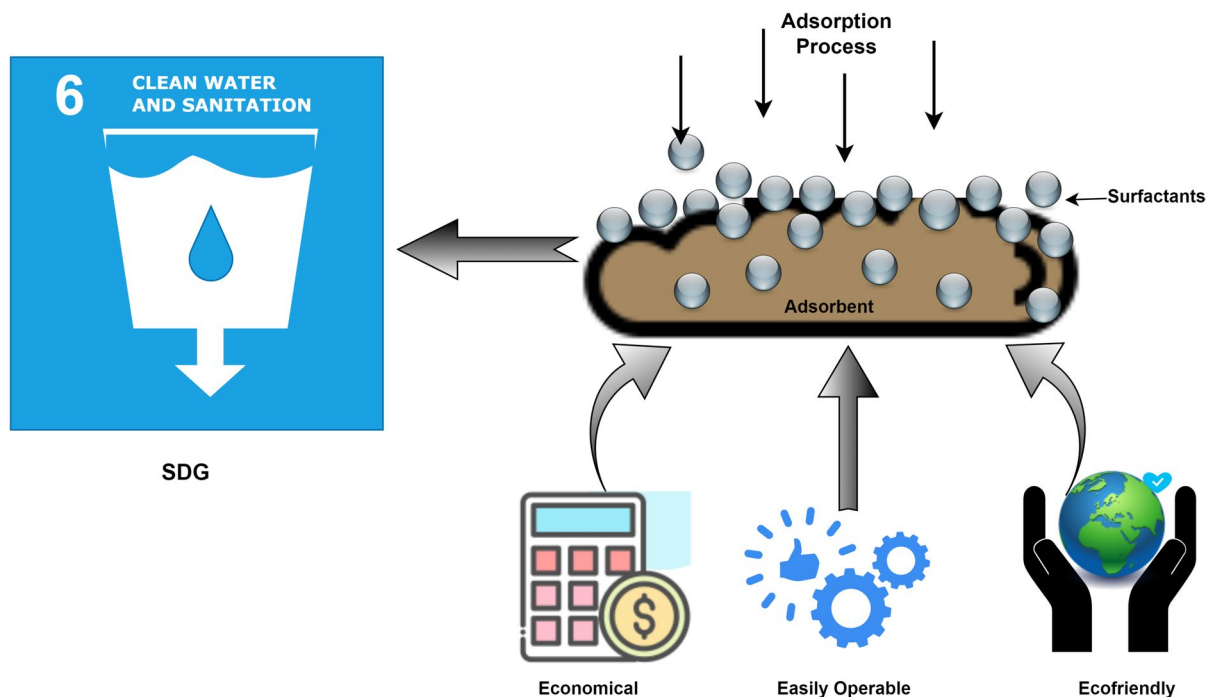


Fig. 1 Adsorption for SDG-6

nature, high surface area, variable surface chemistry, controlled morphological and textural features, make them ideal for the efficient exclusion of organic pollutants through adsorption and photocatalytic degradation (Gusain et al., 2019). Adsorption is a popular method for removing surfactants from wastewater due to its simplicity, excellent efficacy, and low operating costs. Various materials have been used to remove surfactants, including graphene, kaolinite, metal-based composites, nanoparticles, activated carbon and biomass-based adsorbents. Saponite clay and magnetite-based composite sorbents were suggested to have a high surfactant sorption capacity. These magnetic nanocomposite sorbents from clay and magnetite have shown higher effectiveness in wastewater treatment, with two to eight times greater sorption capacities than native clay minerals. These soft magnetic materials efficiently remove spent nanocomposites, making them technologically and economically advantageous solutions (Oksana Makarchuk et al., 2017).

Researchers are now increasingly fascinated by composites as a means of eliminating impurities not only through adsorption but also via flocculation, coagulation, ion exchange, electrostatic interactions, and membrane filtration. Composites are mixtures of two or more distinct component elements that offer product-specific attributes. Grafting, functionalization, and crosslinking are methods for fabricating composites that enhance their characteristics (Dutt et al., 2020). Polymer composites have demonstrated significant potential for implementation in desalination and water treatment processes when combined with other materials, such as carbon-based compounds and clays. These composite materials have enhanced recyclability, selectivity, and adsorption capacity. Depending on the nature of the adsorbent and adsorbate, the adsorption mechanisms involved may be chemisorption or physisorption (Berber, 2020).

Owing to their surface area, functionalization, and chemical approachability, composites must be more widely used than individual materials. Composites are developed by mixing various materials to give them unique characteristics. Composites comprise two distinct phases: a discontinuous dispersion phase and a continuous matrix phase. Composites can provide enhanced qualities like thermal insulation, low density, high specific stiffness, specific strength and

many more. Combining materials with distinct qualities yields new materials with combined features that can be used in many scientific domains, including wastewater treatment (Maqsood et al., 2019; Mushtaq et al., 2019).

The present manuscript attempts to analyse the different surfactant removal methods and adsorbent materials that can be reconsidered, with some modifications, as composites for the efficient eradication of surfactants. A collection, analysis and in-depth review of materials as adsorbents in composites will help researchers working in this domain to easily identify the potential of materials efficient for the remediation of wastewater from surfactants. Such a study has not yet been carried out and is unique.

2 Surfactants in Water

Surfactants and their mixtures are used in various industrial processes, including enhanced oil recovery, flotation, emulsification, corrosion inhibition, drug delivery, cosmetics, and dispersion or flocculation. Such applicability of surfactants is because of their capacity to alter the interfacial properties significantly. Thus, an enormous quantity of surfactants is released daily in the surrounding water bodies. Surfactants in water harm the microorganisms, affecting the overall biodegradation process (James & Ifelebuegu, 2018). Incomplete degradation products of surfactants mimic the hormones of aquatic life, impacting marine life and terrestrial ecosystems (Scott & Jones, 2000). Surfactants constitute a significant hazard to agricultural production and environmental sustainability. They are present not only in domestic and industrial wastewater but also in irrigation water streams being a major constituent of insecticides and pesticides. They may cause soils to become water-resistant and contribute to a decrease in soil hydraulic conductivity. Nearly all forms of water systems in the surrounding environment are now home to surfactants. Their improved solubility and hydrophobic nature reduce the bioremediation rates. All paraffin- or alkane sulfonates, like linear alkylbenzene sulfonates (LAS) and alkylbenzene sulfonates (ABS), are primary surfactants in washing detergents and health care products. Wastewater contains LAS, which prevents bacteria from decomposing organic materials. Cationic surfactants find applications in

shampoos, conditioners for hair, textile softeners, bactericides, and beautifying creams. Because of their effective qualities, surfactants are also known as adjuvants for pharmaceuticals and pesticides (Kulkarni & Jaspal, 2023).

A large quantity of surfactants is now utilized and even further released in marine waters during oil recovery. Thus, the adsorption of these surfactants is crucial not only for more remarkable oil recovery from oil reservoirs but also for avoiding mixing in marine water. Many studies have emerged on surfactant removal by adsorption from oil reservoirs. The surfactant loss resulting from adsorption by the reservoir rocks reduces the oil-water interfacial tension and lowers the chemical effectiveness of the injected slurry. When the percentage of clay minerals in the adsorbents increased by around 5–20 % in the mixture, a direct correlation was observed between the quantity of nonionic surfactants that were adsorbed by the adsorbents and the amount of clay minerals present in the adsorbents (Amirianshoja et al., 2013).

3 Methods for Surfactant Removal

3.1 Biodegradation

3.1.1 Mechanism and Methodical Exploration

Primary biodegradation of surfactant functions when microorganisms structurally modify the parent molecule, resulting in the loss of its surface-active characteristics. The microbes degrade the surfactant, resulting in the formation of products like CO₂, H₂O, and mineral salts. This mechanism is controlled by the type and number of microorganisms, aerobic or anaerobic growth conditions, temperature, pH, nutrients, water content, and substrate bioavailability (Merrettig-Bruns & Jelen, 2009). In wastewater, Surfactants are biodegraded by microbes which consume them to produce energy, nutrients, or catabolism. The procedure of biodegradation is furthermore greatly affected by the chemical composition of the surfactant and the aerobic or anaerobic environmental conditions.

Aerobic degradation method accomplishes better results than anaerobic degradation. During the process of degradation, the high surfactant concentrations depolarize the bacterial cell walls, resulting in

foaming and depriving the air supply. Nevertheless, biodegradation is constrained to wastewater with moderate concentrations, provoking doubts about its utilizations in water bodies with large surfactant concentrations (Palmer & Hatley, 2018). Hence, despite the fact that biodegradation of surfactants is a commonly observed phenomenon for their mitigation in wastewater treatment plants (WWTP), this process alone appears insufficient for successfully and completely removing surfactants. In anaerobic conditions, surfactants comprising fatty acid esters (FES), cationic surfactants, alkyl phenol ethoxylates (APE), fatty alcohol ethoxylates (AE), linear alkyl benzene sulphonates (LAS), and secondary alkyl sulphonates (SAS) are all to a certain degree prone to breakdown during the degradation process. The following represents the order of biodegradation: alkyl sulfates > alkyl ethoxy sulfates > secondary linear alkyl sulfates > primary alkane sulphonates > LAS (Scott & Jones, 2000).

An exploration of the biodegradability of a surfactant (XP-100) with yeast extract, was done in the presence of active hydrocarbon pollutants like naphthalene and hexadecane, revealing that the yeast extract presence accelerated the surfactant biodegradation process, when compared to its absence. Across the examined time frame, increase in surfactant concentration did not prevent its biodegradation. However, addition of organic pollutants enhanced surfactant biodegradation due to their synergistic effect. Compared to hexadecane, naphthalene decomposed more prominently. Surfactants increase the solubility of organic pollutants, making them more bioavailable for bioremediation. Although the surfactants themselves did not appear to be utilized for growth, they significantly contributed to improved biodegradation, by raising the number of pollutants and promoting bacterial growth on organic contaminants. The findings presented an advanced knowledge of the bioremediation process and the destiny of the hazardous organic compounds in the aquatic environment (Aly et al., 1998).

3.1.2 Role of Sustainability

Based on the type of surfactant, aerobic and anaerobic processes play vital roles in its biodegradation. The breaking down of surfactants during biodegradation via microbe's aids in environmental sustainability.

Surfactant metabolites released into nearby water-bodies are often resistant to further breakdown, and mimic the hormones of aquatic organisms. This adversely affects the life cycle of these aquatic organisms. Furthermore, due to their incomplete biodegradation, many surfactants pose severe hazards to the environment. Therefore, though biodegradation appears greener and ecologically sustainable, it is not a reliable surfactant mitigation technique. Since biodegradation is a time-consuming procedure, surfactant removal needs enhancements via standard methods like flocculation and aeration for eco-compatibility. Co-metabolism combined with flocculation or chemical treatments is one of the efficient hybrid approaches that help wastewater treatment facilities remove surfactants (Olkowska et al., 2013).

Biodegradation of LAS from greywater using microbial diversity in constructed wetlands is another trending methodology. In this approach anaerobic conditions dominate the system, with an average LAS and Chemical Oxygen Demand (COD) of 32 mg L^{-1} and 374 mg L^{-1} and removal rates of 43% and 66%, respectively. *Pseudomonas* predominated among the 15 species that degraded surfactants. *Rhodopseudomonas palustris* had the highest relative abundance of operational taxonomic unit (OTU)s in all samples and the highest richness in the anaerobic chamber, among all LAS degraders. Microbial community composition and environmental conditions indicate that LAS biodegradation occurred throughout the constructed wetlands system resulting in a widespread eco-effect. (Mascoli Junior et al., 2023).

3.1.3 Techno-Economic Analysis

Due to their low cost, extended shelf life, and enhanced performance at lower temperatures, petroleum-based surfactants are prominently utilized. However, the exploration for a new ecological, green, biodegradable substitute is essential due to their non-renewability and detrimental environmental impacts. Not only the biodegrading system but also the surfactants are explored to be more sustainable. Hence new biosurfactants are regularly investigated for real time applications. The price of raw materials accounts for roughly 30%–50% of overall biosurfactant production costs. Despite the widespread and environmentally friendly applications

of biosurfactants, the scarcity and high cost of raw materials hinder industrial biosurfactant manufacturing. The market value of biosurfactants was \$1.9 billion in 2022, but the global trend of biosurfactant production mounted dramatically. By 2032, the market is anticipated to reach \$3.2 billion, growing at a compound annual growth rate (CAGR) of 5.4% (Singh et al., 2024).

In the manufacturing of conventional alkyl polyglucosides (APGs) and sucrose esters (SEs) as bio-based surfactants, the review by Stubbs et al. (2022) promotes the use of renewable feedstock, biodegradability, catalysis, atom economy, and safe chemical design as per the green chemistry principles. It encourages the use of bio-based surfactants as more environmentally friendly substitutes. The industry worldwide must create new and sustainable systems, business practices, and technology to promote bio-based surfactants and enhance the commercialization of APGs and SEs. As a conceivable substitute for synthetic surfactants, green surfactants such as biosurfactants and oleo surfactants, are being synthesized as a result of biotechnological advancements and are becoming more and more popular globally (Nagtode et al., 2023).

The commercial viability of anaerobic membrane bioreactor (AnMBR) integrating with forward osmosis (FO), reverse osmosis (RO) technologies for municipal wastewater treatment with energy and water generation was considered. AnMBR facilitated for wastewater treatment and energy generation, while RO aided in water production and draw solution regeneration. The FO assisted with pre-concentration of the AnMBR influent. Restraining the FO recovery to 50% in a closed-loop approach resulted in a minimal wastewater treatment expense of $0.81 \text{ euros m}^{-3}$. FO recoveries of 80% and 90% resulted in higher costs of 1.01- and 1.27-euros m^{-3} , respectively. The projected costs for producing fresh water were 0.80 and 1.16 € m^{-3} for a closed-loop strategy and an open-loop scheme that maximized water output, respectively. It was suggested that the FO membrane fluxes of 10 LMH would significantly increase the effectiveness of AnMBR technology and FO-RO. According to a sensitivity analysis, the low FO membrane fluxes were observed as a limiting factor (Vinardell et al., 2020).

3.1.4 Limitations, Industrial Applications and Future Advances

The increased utility of surfactants and the available degradation setups at the wastewater treatment plants show inconsistent and time-consuming results. Nevertheless, many attempts have been made to enhance the impact of biodegradation, especially associated with foul smell. In one such effort, the impact of ethyl alcohol and nitrate on the degradation of linear alkylbenzene sulfonate (LAS) was examined utilizing a central composite design (CCD). The CCD technique proposes a tool for optimizing processes and determining the significance of elements influencing them. It assists to understand process functionality and its application in industrial reactors on a small scale after defining optimal parameters. Nitrate and ethanol (co-substrate) affect in almost complete decomposition of surfactants, overcoming the fundamental limitation. Ethanol and nitrate substantially impact ($p < 0.05$) on the degradation of linear alkylbenzene sulfonate in batch reactors. 99.9% LAS was removed with ideal values of around 97.49 and 87.99 mg L⁻¹ for ethanol and nitrate, respectively, under agitation at ≈ 119.9 rpm and 29.8°C (Andrade et al., 2017).

An extended granulated sludge bed reactor meant for the anaerobic digestion of domestic and commercial laundry wastewater was assessed at three stages, with a 36-hour hydraulic retention period. Tap water and mixing domestic sewage were used to dilute the wastewater stream. A reduction in the LAS exclusion rate from about $77 \pm 15\%$ (stage I) to around $55 \pm 18\%$ (stage III) resulted from the addition of domestic sewage, which raised LAS and organic compounds concentration in the influent. Thus, a substantial decline in the rate of LAS removal and an association between LAS removal and specific organic loading rate were revealed by data analysis, posing another limitation in removal of surfactant (de Faria et al., 2019).

Therefore, in order to overcome this issue, the microalgal-bacterial processes were employed by high-rate algal pond (HRAP) systems to eliminate surfactants and other pollutants from household wastewater efficiently. In HRAPs, *Scenedesmus* sp. algae was introduced at concentrations of 1.4 g L⁻¹ for total suspended solids (TSS) and 4.2 g TSS L⁻¹ for activated sludge. In three high-rate algal ponds, the feeding schedule affected the removal of surfactants,

nutrients, and biomass production. At 0.1h d⁻¹, the best results were obtained, with surfactant concentrations of 0.3 mg L⁻¹ below the permissible limits for freshwater outflow (Serejo et al., 2020).

Peroxymonosulfate (PMS) was activated using sludge-derived biochar (SBC) to break down triclosan (TCS), a surfactant, in wastewater. SBC had a specific surface area of around 158 m²g⁻¹ and a porous structure. The ideal conditions for triclosan (0.034 mM) degradation in the activated SBC- PMS system was pH 7.2, with 0.99 g L⁻¹ of SBC, and 0.79 mM of PMS at 25°C. The results showed that SBC can serve as a useful PMS activator for the breakdown of surfactants in water and wastewater, with a TCS removal effectiveness of 66.7%, significantly better than the contributions of pure SBC and PMS (Wang & Wang, 2019).

Recent studies evidently suggest that oilfield dispersants build up in the water column and sink with oil to the sea bottom, particularly affecting the extremely delicate coral reefs and hazarding the marine ecology. Hence, the biodegradability of oilfield detergents comprising anionic surfactants was tested for water samples from the New Calabar river of the University of Port Harcourt, Nigeria, and the tap water was obtained from the laboratory taps. The detergents examined were Bio-Boost, SUR-500 (SURFONIC® OFS 500 polyol), a dispersant SW-1000, drilling detergent D.D-Y, and degreaser D.G-X. This analysis employed to track the biodegradation of methylene blue active substance (MBAS) while utilising sodium dodecyl sulphate (SDS) as a reference, signifying a biodegradation observation practice. *Proteus*, *Acinetobacter*, *Enterobacter*, *Staphylococcus*, *Bacillus*, *Pseudomonas*, *Arthrobacter*, *Corynebacterium*, and *Micrococcus* were the microorganisms that used the detergent. The detergents met biodegradability criteria with an average primary biodegradation rate of 91%–97 % (Osadebe et al., 2018).

3.2 Coagulation and Flocculation

3.2.1 Mechanism and Methodical Exploration

Coagulation and flocculation are vital processes in wastewater treatment, employed together on the principle to eliminate suspended particles by destabilizing them, causing them to clump together. As a result, these processes further facilitate effortless removal

of the suspended water impurities like surfactants through sedimentation or filtration. Surfactant molecules consist both hydrophilic and hydrophobic ends and Anionic and nonionic surfactants can both be eliminated by coagulation (Amir Hossein et al., 2004). The coagulation mechanism for surfactant elimination involves neutralizing its charges and promoting accumulation. Coagulation-flocculation techniques can often achieve high removal rates while effectively lowering surfactant concentrations in wastewater. Adsorptive micellar flocculation (AMF) is a surfactant-based separation technique that eliminates water-soluble contaminants. In this technique first the contaminants in surfactant micelles are dissolved, which eventually flocculate and then precipitate out of the solution. The ability of surfactants to produce micelles, encapsulating and concentrating contaminants, is thus employed for their removal, in this procedure. The addition of polyvalent cations causes flocculation, amassing the micelles into bigger flocs that are readily removed by sedimentation or filtration. Due to its exceptional pollutant removal efficiency, coagulation-flocculation unit processes in wastewater treatment, has appealed significant consideration (Aboulhassan et al., 2006).

According to previous studies, ferric chloride, alum, and lime have commonly been used as coagulants. The survey by Jangkorn et al., 2011 examined the viability of recycling aluminum sulfate (alum) sludge as a coagulant or coagulation aid to reduce new alum dosage and improve removal efficiency. Experimentations were conducted in a jar-test system to simulate the coagulation-flocculation process for removing organic matter, anionic surfactants, suspended particles, and turbidity. The results demonstrated that alum sludge could effectively eliminate turbidity, Total Chemical Oxygen Demand (TCOD), and anionic surfactants at an initial pH of 10 and a fresh alum content of 400 mg L^{-1} . The use of both alum sludge and fresh alum improved the removal efficacy. The TCOD removal efficiency exceeded 80%, which was never achieved with fresh alum alone. The study suggests that alum sludge can be recycled to remediate industrial wastewater from the consumer goods industry. Another study by Tripathi et al. (2013) revealed that the electrocoagulation-electroflotation approach effectively removes residual surfactants from laundry wastewater, reducing COD by 80%, MBAS by 95%, and turbidity by 99.9%.

3.2.2 Role in Sustainability

Chemical coagulants are effective in surfactant treatment from water treatment plants (WT), but they are typically costly, hazardous, and responsible for health problems, and therefore not sustainable. Natural coagulants are a renewable substitute as they are easily accessible, affordable, simple to use, biodegradable, non-toxic, a greener approach to environmentally benign chemicals, efficient, and produce smaller volumes of sludge (Banchon et al., 2017; Turk et al., 2005). Natural coagulants, through an adsorption process similar to chemicals, and have a WT efficiency of 50-500 nephelometric turbidity units (NTUs). These coagulants can contribute to several health issues in developing countries. However, their acceptance, commercialization, and widespread industrial application are still low (Koul et al., 2022). When using *Cicer arietinum* powder as a bio-coagulant, the ideal coagulation and flocculation parameters were 2.26 g L^{-1} of coagulant, $\text{pH} = 4$, and flash mixing speed = 170 rpm. Turbidity, surfactant, and chemical oxygen demand (COD) removal efficiencies under this environment were $88.35 \pm 4.10 \%$, $60.30 \pm 3.10 \%$, and $54.25 \pm 2.81 \%$, respectively. Thus, there is an urgent need to accept and commercialise natural coagulants like *Cicer arietinum* as a sustainable substitute to chemical coagulants (Dadebo et al., 2022).

To consider the process of coagulation and flocculation from the aspect of sustainability and green chemistry, an innovative green coagulant, like flax-seed mucilage (FSM), was used by Mirbahoush and his team in 2019. The optimal conditions for coagulation of anionic surfactant sodium dodecyl sulphate (SDS), employing the response surface methodological approach were a pH of 7.0, 100 mg L^{-1} of FSM, and 30 min. Heterogeneous photo-Fenton oxidation was employed in the post-treatment phase to ensure the complete removal of SDS using an MnFe_2O_4 nanocatalyst. Complete SDS removal was accomplished in the photo-Fenton oxidation process with 76 mg of the nanocatalyst and 1.07 mL of H_2O_2 at 17 min. Coagulants and flocculants are also further associated with changes in the chemical compositions of water bodies and are not entirely reliable.

3.2.3 Techno-Economic Analysis

Coagulation flocculation, though a simple, selective, and cost-effective method for treating wastewater, desires concern for the toxic by-products. Applying adsorptive micellar flocculation (AMF) directly to wastewater does not cause any eco-toxicity, and hence makes it a simple, selective, and economically feasible process. To treat industrial wastewater with a high concentration of surfactants, Aboulhassan et al., in 2006 investigated the effectiveness of the coagulation precipitation process worked, especially in terms of eliminating organic debris and surfactants. In this study, the treatment with FeCl_3 was found effective at the pH range of 7–9. In addition to increasing the BOD_5/COD index from 0.17 to 0.41, the procedure successfully reduced surfactants and COD, with improved removal rates of 99% and 88%, respectively.

A study investigated electrochemical coagulation utilizing Fe^{2+} ions as an alternative method for removing surfactants from water samples and model solutions. The results showed that a concentration of 10 mg L^{-1} of surfactant was removed with 100% efficiency. The study also examined the impacts of applied current density, initial concentration, supporting electrolyte concentration, coagulant dosage, and pH on removal efficiency. This suggested that electrochemical coagulation is a promising method for treating detergents polluted water. The high concentration of iron hydroxide near the anode enhanced the coagulation of pollutants, while the negative electrode caused rapid floc movement, which did not significantly enhance coagulation. Energy consumption was lower when the reactor was anode. Evidently demonstrating a lower energy utilization technique. However, generating water with 1 mg L^{-1} surfactant is more expensive than producing 2 mg L^{-1} water, and should be considered for the economic evaluation of the process (Önder et al., 2007).

Eradication of anionic surfactants from wastewater from the cardboard industry using coagulation-flocculation was analysed. It was observed that the statistical approach of response surface methodology enables an efficient and cost-effective study of the interactions between diverse parameters used in coagulation-flocculation. With the use of cationic polyacrylamides (c-PAM), poly aluminium chloride (PAC), and pH at optimal levels, coagulation-flocculation eliminated the anionic surfactant nearly

entirely and decrease COD by more than 95% (Harif et al., 2023). Electrocoagulation and electroflotation were used in a study by Akarsu and Deniz (2021) to investigate wastewater treatment from laundry. The response surface methodology (RSM) was utilized for optimizing the type of electrode (Al–Al, Al–Fe, Fe–Fe, and Fe–Al), initial pH (5–9), current (0.54–2.16 A), and time duration (15–60 min). Using a Fe–Al electrode at 2.16 A current at pH 9 and 60 min reaction time results in the most efficient elimination. The techno-economic study thus revealed that at an operating cost of $\$1.32 \text{ m}^{-3}$, the best removal efficiency is obtained for COD, colour, surfactant, and microplastic.

3.2.4 Limitations, Industrial Applications and Future Advances

The efficiency of the coagulation-flocculation method depends on the coagulant dose and pH of system. Coagulants also generate harmful sludge adding to the impurities in water. As a result, additional filtration is necessary for complete mitigation of the contaminants in the sludges. Chemical hazards of coagulant material are another matter of great concern. The coagulation-flocculation is a regularly used process to treat industrial wastewater produced while manufacturing detergents, soaps, and other consumer goods and adding coagulators and utilizing chemicals to change the pH of these industrial effluents incurs a substantial cost. To decrease the quantity of fresh alum required and to improve the efficiency of the removal process, a study was conducted to see whether the aluminum sulfate (alum) sludge might be used again as coagulant or a coagulation aid. Examinations were carried out in flocculators to eliminate turbidity, suspended particles, organic debris, and anionic surfactants. An optimal starting pH of 10 and the addition of 400 mg L^{-1} alum resulted in the removal efficiencies for TSS, COD, anionic surfactants (AS), and turbidity within a range of 70–98% (Jangkorn et al., 2011) suggesting these as the optimum parameters for effective removal.

Recent innovative trends in this sector recommended a microbubble-enhanced flotation approach that successfully removed over 95 wt. % of surfactants, from laundry wastewater (Zhao et al., 2024). Polyacrylamide (PAM) was also discovered to be an effective coagulant aid for polymeric

aluminium chloride (PAC) to increase floc characteristics in a dual-coagulation procedure used for surfactant-kaolin wastewater (Li et al., 2024). *Moringa oleifera* shows notable coagulation skills far earlier than other recently used bio coagulants like *Cicer arietinum* (Dadebo et al., 2022) and flaxseed mucilage (Mirbahoush et al., 2019). *Moringa oleifera* seed extract was shown to remove surfactants from aqueous effluents effectively. Among them, Polyoxyethylene (3.5) sodium lauryl ether sulfate (SLES), a long-chain anionic detergent, was chosen as an exemplary molecule to evaluate the coagulation reaction. The system coagulant-detergent demonstrated high efficacy and stability across various temperatures and pH levels. The *M. oleifera* promises as an efficient coagulant, with a coagulation capability of 0.245 mg L^{-1} . Experiment design identified the optimal coagulant dose and initial concentration of surfactant as 234 mg L^{-1} and 76 mg L^{-1} , respectively (Beltrán-Heredia et al., 2012). Further, research is therefore crucial to explore the mode of action, adoption, and commercialization of similar natural coagulants as a sustainable alternate for a circular economy.

3.3 Photocatalytic Degradation or Advanced Oxidation

3.3.1 Mechanism and Methodical Exploration

Photocatalytic degradation, an advanced oxidation process (AOP), incorporates light energy in presence of a catalyst and converts pollutants into innocuous molecules such as CO_2 and water by producing reactive oxygen species. Photocatalytic techniques effectively treat waterbodies contaminated with organic and inorganic contaminants. Photocatalytic procedures operate to mineralize a wide range of surfactants along with many insecticides, dyes and other such hazardous chemicals. The use of photoactive semiconductors is a favorable approach for these methods. For photocatalytic applications, titanium dioxide is the most commonly utilized semiconducting material. Combining TiO_2 -based photocatalysis and sonolysis is a potential mechanism for reducing organic contaminants like surfactants (Szabó-Bárdos et al., 2008). Advanced oxidation process (AOP) yields extremely reactive intermediates known as hydroxyl radicals ($\text{HO}\bullet$) by utilizing strong oxidants such as O_3 or H_2O_2 . This hydroxyl radical breaks

down the organic compounds quite efficiently. Surfactants, including all other organic molecules, are essentially disintegrated by the ($\text{HO}\bullet$) once it is created. As a result, the organic component mineralizes due to hydroxyl radical assault. Thus, organic pollutants are reduced by AOPs from several hundred parts per million to fewer than five parts per billion. The AOP generates an organic radical ($\bullet\text{R}$) by removing a H atom from an organic molecule (RH) using ($\text{HO}\bullet$). Numerous oxidation products are produced due to the several chemical changes the organic radical ($\bullet\text{R}$) goes through. Fenton's reagent ($\text{H}_2\text{O}_2\text{-Fe}^{2+}$), O_3 , and H_2O_2 are the most often utilized oxidants in AOP (Krishnan et al., 2016).

A hybrid treatment system mechanism was designed to treat synthetic wastewater spiked with $10.00 \pm 0.46 \text{ mg L}^{-1}$ sodium dodecyl sulfate (SDS), including an up-flow microbial fuel cell (MFC) with TiO_2 or titanium dioxide as a photocathode catalyst. After passing through a raw laterite sand filter, the anodic chamber of the MFC's effluent was followed by a photo cathodic chamber with a UV-exposed TiO_2 -coated cathode. The hybrid system was run in an MFC anodic chamber for varied hydraulic retention times (HRT). The hybrid system achieved over 96% removal efficiency of SDS and $\approx 70.99\%$ removal efficiency of organic materials at various HRTs (Sathe et al., 2020).

3.3.2 Role in Sustainability

The photocatalytic technique oxidizes the water pollutant in a more sustainable and efficient sequence of processes. The method is used to effectively decontaminate and sterilize wastewater and sanitize groundwater. Wastewater, including surfactants, heavy metals, medications, chlorinated hydrocarbons, pesticides, dioxins, diseases, and microorganisms, a widespread of water impurities can be treated by photocatalytic oxidation. The photo-catalytic methodology is more practical, energy-efficient, and chemical-free than traditional oxidation techniques. Additionally, photocatalytic degradation works at moderate temperatures and pressures, and the method becomes more effective when heterogeneous photocatalysts are used (Ahtasham Iqbal et al., 2024), suggesting sustainable and readily available application conditions. Photocatalysts can alter the chemical compositions of water reservoirs during treatments (Joseph et al., 2022).

Hence, the appropriate selection and use of reagents associated with green chemistry is necessary for sustainable wastewater treatments.

Structural effects of surfactants lead to the development of photodegradation products with higher toxicity than the parent molecule. Recently, catalytic photodegradation of cationic, anionic, and non-ionic surfactants was explored by Wysokowska et al. (2024) to determine the effect of their breakdown products on phytotoxicity of sorghum (cereal grain). As a result, heterogeneous photocatalysis successfully mitigates surfactants only at low concentrations in the aquatic environment. Photodegradation efficacy for all surfactants improved proportionally to a range of 41–50% for anionic surfactants, 64–70% for non-ionic chemicals, and 38–43% for cationic cetrimonium bromide (CTAB) and Didecyl dimethyl ammonium chloride DDAC, while the efficiency of benzalkonium chloride reached 94%. Non-ionic surfactants provided the finest toxicity reduction outcomes, followed by anionic chemicals, whereas cationic surfactants were correlated with a more substantial negative impact adding to more toxicity. In contrast to anionic and non-ionic chemicals, cationic compounds degrade more slowly due to their decreased reactivity, which is hampered by their positive charge, thus affecting the phytotoxicity.

3.3.3 Techno-Economic Analysis

Surfactant removal is a developing concern due to its stubborn nature, which hinders conventional biological treatment from meeting wastewater discharge standards. A laboratory-scale photocatalytic degradation system employing UV-H₂O₂ was recommended as an additional treatment for a mixed multiple anaerobic system facility in Guayaquil, Ecuador, which had inadequate surfactant removal (45.9%). The system proved the synergistic effect of mixing H₂O₂ with UV radiation for 60 min in successfully removing surfactants (94.3±4.3%) and reaching the treatment objective. After 60 min of continuous treatment with a flow rate of 0.6 mL s⁻¹ and a hydrogen peroxide concentration of 26.6 mg s⁻¹, the highest elimination of anionic surfactant was 92.3±2.5%. The techno-economic analysis of this study estimates that removing surfactants in an ideal full-scale system, combined with a decentralized wastewater treatment plant would cost 0.7 \$ m⁻³ (Jennifer et al., 2024).

Recently, electron beam radiation, a clean and sustainable method for SDBS degradation in wastewater, was explored by Chu et al. (2024). Changes in SDBS micelles, elevated interfacial tension, and reduced foaming power resulted from the breakdown process. With a COD removal rate of 7–20%, the results demonstrated a removal efficiency of almost 100%. Advanced electro-oxidation has become a predominant method for treating complex wastewater. For domestic wastewater effluent from the wastewater treatment facility in Ecuador, an electrochemical degradation method employing a *DiaClean*® cell in a recirculating system with boron-doped diamond (BDD) as the anode and stainless steel as the cathode was found to be economically beneficial (Cisneros-León et al., 2023).

3.3.4 Limitations, Industrial Applications and Future Advances

The requirement for large space, high operation expenses, high reagents utilization, and high energy requirements are the commonly observed limitations of photocatalytic techniques. Municipal effluent samples and distilled water-spiked samples containing 100 mg L⁻¹ of SDS were tested for an advanced oxidation process employing UV-H₂O₂. The impacts of process parameters on SDS degradation, such as latency, initial SDS concentration, oxidant H₂O₂ dosage, and UV absorbance of wastewater at 250 nm, were analysed. The rate of SDS breakdown increased with reaction time. Depending on the initial SDS concentration, degradation accelerates with increasing oxidant dose and decreases even further with growing oxidant dose. This confines that degradation does not increase with increasing the oxidant dose. Through 200 mg L⁻¹ of initial concentration, the quadratic model predicted that the maximum SDS degradation percentage would be over 80% in 7 min. For the same, a UV absorbance of around 0.2 at 254 nm was obtained using a dosage of 2 mol of H₂O₂ per mol of SDS (Mondal et al., 2019).

The effectiveness of the electro-hybrid ozonation-coagulation process (E-HOC) for surfactant and microplastic exclusion from laundry wastewater was investigated at various current densities and ozone dosages. At ideal circumstances (current density 15 mA cm⁻², ozone dosage 66.2 mg L⁻¹), surfactant and microplastic removal efficiency exceeds 90%. The E-HOC method has a better exclusion efficiency of COD, turbidity, and

LAS than the ozonation and conventional electrocoagulation processes proposing a better practical approach. The electro-hybrid ozonation-coagulation process was optimized for three laundry wastewaters: washing wastewater (15 mA cm^{-2} , 66.2 mg L^{-1}), primary effluent (10 mA cm^{-2} , 36.6 mg L^{-1}), and secondary effluent (10 mA cm^{-2} , 36.6 mg L^{-1}). COD, turbidity, and LAS were removed from washing wastewater at rates of 93.9%, 99.7%, and 99.9%, respectively (Luo et al., 2022).

Photocatalytic degradation combined with adsorption is a hybrid approach boosting traditional yet affordable processes. As surfactants are discharged into wastewater in huge quantities, they are detrimental to aquatic and terrestrial life, necessitating removal. A recent study attempted to eliminate SDS surfactant through photocatalytic degradation and adsorption utilizing Zn (+2) Al-layered double hydroxide and TiO_2 -Zn (+2) Al-layered double hydroxide coprecipitation materials. The acquired experimental results were analysed using the Temkin and Langmuir and the Freundlich adsorption isotherm models. The photocatalytic degradation of SDS over Zn (+2) Al-layered double hydroxide and TiO_2 -Zn (+2) Al-layered double hydroxide exhibited pseudo-first-order kinetics at 9.99 to 100.1 mg L^{-1} concentrations. The results showed that $\text{TiO}_2(3.59)$ -Zn (+2) Al-layered double hydroxide displayed substantial photocatalytic activity compared to the Zn (+2) Al-layered double hydroxide sample (Aoudjit et al., 2019).

Photocatalytic degradation is a developing trend that is globally used for surfactant removal to achieve water remediation. Lately, photocatalytic degradation combined with adsorption on Fe_2O_3 -activated carbon catalyst was found effective in the degradation of surfactants like linear alkylbenzene sulfonate. When the concentration of Fe is changed to 2%, 4%, or 6%, the capacity of the surfactant waste degrading reaction using the kernel of coconut catalyst at a time frame of three hours was determined to be nearly 6.8 mmol g^{-1} , 3.2 mmol g^{-1} , and 1.6 mmol g^{-1} catalyst, respectively (Amelia et al., 2020).

3.4 Membrane Filtration

3.4.1 Mechanism and Methodical Exploration

Porous membranes featuring specific pore diameters are used in membrane filtration methodology.

Surfactants develop micelles or other more significant structures, depending on their concentration and degree of aggregation. These aggregates are physically confined and unable to flow through the membrane as their size exceeds the membrane pore size. This isolates them from the water stream. The size exclusion mechanism is the key component in separating surfactants from water in microfiltration (MF) and ultrafiltration (UF) procedures, where the pore diameters range from micrometres to nanometers (Xiarchos et al., 2003). Utilizing a semi-permeable membrane, the filtration technique employs a pressure differential phenomenon to separate components in aqueous solutions. This pressure difference mechanism permits smaller molecules to flow through, thus retaining bigger molecules in situ. The technique is based on factors including size, molecular properties, or charge. As a pre-treatment technique, membrane filtration (MF) is frequently used to remove various components from wastewater suspension, whereas ultrafiltration (UF) suggests a way to eliminate surfactants from aqueous solutions with critical micelle concentration (CMC). Nevertheless, nanofiltration (NF) is a more successful removal method when the concentration is as low as that of monomer. Because of the high concentration of surfactant monomers, the membrane filtration technique enables the permeate to be reused during the cleaning process. In the early 1970s, UF was the first membrane technique to separate surfactants (Suárez et al., 2012).

Composite membranes of silica, titania nanorods, and nanotubes, with photocatalytic capacity, were explored to remove sodium dodecylbenzene sulfonate (SDBS). Using the sol-gel method, colloidal silica-titania sols have effectively created a multifunctional composite membrane. Blending photocatalysis with membrane filtration was an innovative trial that resulted in an 89% elimination of SDBS after 100 min, according to the experimental results (H. Zhang et al., 2006). Babaei and team in 2019 (Babaei et al., 2019) studied the effectiveness of multi-layer slow sand filter, microfilter (MF) and ultrafilter (UF) hybrid systems in removing COD, TSS, LAS and turbidity from greywater, and the impact of OLRs on the performance of the system during 5 months. The finest removal efficiencies were 98.22% for COD, and >99.97% for TSS, LAS and turbidity also. Furthermore, the average turbidity, TSS, and LAS outputs in

the hybrid system were 1.04 NTU, 0.04 mg L⁻¹, and 1.55 mg L⁻¹, respectively.

To treat surfactants from detergent wastewater, a combination method using the multimedia biological aerated filter (MBAF) and the up-flow multimedium biological aerated filter (UMBAF) was studied by Ji et al. (2019). The combined system had an optimal filtration rate of 1.4 m hr⁻¹ and performed best with an air-to-water ratio of 2:1. Total phosphate (TP), linear alkyl benzene sulfonate sodium (LAS), and Chemical Oxygen Demand (COD) were removed at average rates up to 40%, 88%, and 91%, respectively.

3.4.2 Role in Sustainability

Growing international apprehension about scarcity of clean water and environmental sustainability drives revolution in water reclamation techniques. Research by Barambu et al. (2020) reveals the ability of a tilted panel system to maximize the impact of air bubble contact with the membrane surface, hence imposing control over membrane fouling and emerges as a greener methodology. This technology offers a simple method for recovering detergent and reusing water. Hydraulic performance improves when rate of aeration and tilting angle are adjusted to attain permeability, implying that almost all reversible fouling can be avoided. The plateau aeration resulted in a 83% higher permeability than the unaerated condition, with value of about 200. Tilting the membrane panel 15 degrees to the air bubbles increased permeability to around 220. The method further provides 32% detergent recovery. Overall, the technique proposes a compelling method for membrane fouling management.

Research by Mostafazadeh et al. (2019) focuses on the treatment and reuse of laundry wastewater utilizing an innovative and sustainable sequential integrated system. Total suspended particles, turbidity, COD, and surfactants such as nonylphenol ethoxylates (NPEO₃-17) are eliminated by polyether sulfone (PES) membrane in ultrafiltration (UF) of raw wastewater and adsorption (AD) procedures of the filtrate. The UF process separates the wastewater into an effluent with a minimal organic pollutant; ≈400 mg L⁻¹ of dissolved COD, and a concentrate with a total COD upto 1200 mg L⁻¹, with around 200 mg TSS L⁻¹. Thus, using UF and AD procedures, successfully eliminates NPEO₃-17 surfactant from the concentrate and filtrate efficiently.

3.4.3 Techno-Economic Analysis

Recently a microfiltration membrane system with cationic exchange proceeding a weak-acid-based resin was proposed to eliminate surfactants and lower effluent alkalinity from the washing phase. The recovery efficiency of the system was 88%. About 68% of the cooling tower water was treated using the ultrafiltration and reverse osmosis processes, which were determined to be the most successful in eliminating salts and biocides. The techno-economic feasibility for the system was assessed, with an anticipated cost of EUR 245 thousand for the washing phase and EUR 582 thousand for the cooling towers. The revenue from the treatment techniques was expected to be EUR 0.07 per car for the washing phase and cooling towers with EUR 0.13. This study highlights the benefits of membrane treatment in the environmental policy of the automotive sector, leading to water reuse and lower effluent discharge (Carvalho et al., 2025).

As per a survey by Šostar-Turk et al. (2005), Slovenia implemented two initiatives that enforced technological and ecological standards for treating wastewater from modern laundry. On examining prospective market for membrane water treatment applications, it was discovered that most Slovenian laundering facilities, out of 140 at that time, employed traditional techniques such as filtration, flocculation, and sedimentation. Only three laundries with annual water flows ranging from 35,000 to 45,000 m³ had ultrafiltration installed. To resolve this issue, a membrane treatment system combining ultrafiltration and reverse osmosis was developed in a laboratory, enabling 75% of water to be recycled. Ten prospective laundries in Slovenia were found qualified for this system, with five having water flows ranging from 35,000 m³ to 100,000 m³ per year.

3.4.4 Limitation, Industrial Applications and Future Advances

Despite the beneficiary membrane filtration treatment on effluent from laundry, particularly when reusing water and detergent, membrane fouling and regeneration significantly limit its performance, particularly when operated at high transmembrane pressure. Chemical resistance and strength of the membrane are crucial factors affecting filtration methods. Hence recently, Bilad et al. (2020) conducted research to

evaluate a low-pressure immersed membrane filtration system for processing wastewater from laundry to overcome the fouling issue. A solution of 15 wt% polysulfones, 1 wt% polyethene glycol, and dimethylacetamide was employed to fabricate the membrane in this analysis. This polymeric membrane promises efficient elimination of surfactant turbidity, total nitrogen, phosphorus, and chemical oxygen demand of 52%, 13%, 65%, and 97%, respectively. The system additionally offers 78% detergent recovery from spent laundry effluent, proving its potential.

Unique modules of ceramic membrane with a pore size of 0.14 μm can demonstrate high efficacy in surfactant wastewater treatment, reducing TOC, COD, and turbidity by 95%, 93%, and 99%, respectively, when the process was run in concentration mode, resulting in the recovery of nearly 50% of the permeate. The study examines the composition of industrial wastewater, its purification, and concentration processes using the modules of ceramic membrane. The wastewater was produced from a plant that manufactures cationic surfactants and was exposed to membrane filtration in a semi-pilot plant. The regeneration operation using NaOH solution was successful, although the permeability of the module was not fully restored. Applying an acidic washing agent can reduce the intensity of membrane blockage. Filtration tests with model solutions confirmed that the sieve effect dominates surfactant separation during UF and MF processes. Modules with their pore diameters similar to or smaller than the size of the surfactant micelles (150 kDa and 0.45 μm) have more significant retention coefficients (above 94%). They are less susceptible to surfactant fouling (Klimonda & Kowalska, 2021).

In order to remove 18 per- and poly-fluoroalkyl species (PFAS) from drinking water, Johnson et al. (2022) proposed an amphiphilic coating to functionalize aluminum oxide hydroxide membrane. Eleven of the 18 PFAS in the challenge water were removed with >99% efficiency using dynamic filtration. Fifteen were removed with greater than 90% efficiency using gravity filtration. For perfluorooctanoic acid adsorption capacity, the novel amphiphilic coating performs better than granular activated carbon (GAC) under dynamic filtering conditions, and even better for perfluorooctane sulfonic acid. The free energy, enthalpy, and entropy of interactions between six

PFAS pollutants and coatings were calculated using molecular dynamics simulations.

Membrane-based technologies provide a novel approach for reclaiming water from laundry wastewater (LWW), with pollutants being removed at an efficiency of 85–95% when appropriately adjusted. These systems are adaptable and provide water that is suitable for laundry reuse. Investigate advancements in both independently operable and hybrid membrane systems for treating LWW. Membrane-based techniques can remove critical LWW components such as surfactants and suspended particles. The combination of membrane processes and conventional techniques improve performance by 45–50% while reducing energy consumption by up to 25% (Zakaria et al., 2025).

4 Adsorption for Surfactant Removal

4.1 Mechanism and Methodical Exploration

Surfactants primarily adsorb on adsorption surfaces by electrostatic attraction and van der Waals forces. The cationic surfactant adsorbs when the positive charge on its headgroup attracts negative charges on the adsorptive surface. Anionic surfactants with a negative charge on their headgroup and the positively charged adsorptive surface may be attracted to each other electrostatically. The principal adsorption mechanism for nonionic surfactants is hydrogen bonding (Kalam et al., 2021b, 2021a). Surfactant adsorption, or the concentration of surfactant molecules at interfaces, is triggered by various forces comprising electrostatic attraction, hydrophobic interactions, and hydrogen bonding. It is further contingent on the surfactant and surface attributes (Siyal et al., 2020). Adsorption depends on various physicochemical properties of the adsorbents and the surrounding atmosphere. Pore size, temperature, adsorbent dose, the concentration of surfactant to be removed, pH, and functional groups on adsorbents are the common governing factors for adsorption. One such comparative study showed that adsorbents and ion exchange resins with functional groups impede mass movement of the surfactant perfluoro-octane sulfonate (PFOS), which lowers the sorption rate. The sequence in which the total PFOS capacities of adsorbents rise is polymer adsorbents > activated carbons > anion exchange resins; the selectivity of functional groups influences the

adsorption process (Schuricht et al., 2017). Surfactant adsorption on polymers is crucial for maintaining polymer latex colloidal stability. Ionic surfactants bind neutral polymers through hydrophobic interactions, whereas oppositely charged polymers bind surfactants through electrostatic and hydrophobic interactions. The efficiency of surfactant adsorption depends upon the capacity of the polymer surface and the molecular structure of surfactants. The hydrophobicity of the polymer surface, its ionic nature, its curvature radius, the structure of the surface-active material, and the bulk fluid phase parameters such as temperature and electrolyte concentration are the factors governing adsorption (El Feky et al., 2010).

Various minerals and soil types also facilitate surfactant removal. A study observed the extent of adsorption of anionic surfactant and amphoteric surfactants betaine and sulfo-betaine during oil recovery. Adsorption of ionic surfactants on sandstone and dolomite was lower than that of amphoteric surfactants, while amphoteric surfactants adsorbed similarly or lower on limestone. Adsorption of anionic surfactants followed an electrostatic mechanism, while amphoteric surfactants adsorbed through a complex interplay (Mannhardt et al., 1992).

As adsorbents play a vital role in the adsorption of surfactants, some major adsorbents with implemented modifications used previously for surfactant removal are listed in Table 1

4.2 Role in Sustainability

Biodegradable adsorptive materials, including biomass or biopolymers, are essential for protecting the environment, especially in wastewater treatment. Biopolymers, like chitosan, alginate, and tannin composites, have shown potential as attractive adsorbents for the future. They may substitute traditional adsorbents like silicates, aluminates, and activated carbon, offering competing adsorption capacity, cost-effectiveness, and biocompatibility. However, their applications for wastewater treatment have not been thoroughly explored, indicating a need for further exploration (Biswas & Pal, 2021). Sen et al. (2012) used pine cone biomass to remove sodium dodecyl sulfate, an anionic surfactant. Using *Posidonia oceanica* (L.), a cheap, plentiful, and renewable marine biomass, adsorption has been used in batch mode to remove anionic and non-ionic surfactants (Ncibi et al., 2008).

Post-treatment of primary and secondary sewage wastewater utilizing slow sand filtration and adsorption by activated carbon (AC) made from eco-friendly residual coffee dregs reduced surfactants and turbidity by approximately 95% and 94%, respectively (Marcelo & Alexandre, 2021). Lately, Nacar et al. (2022) successfully removed up to 90% of detergent (Sodium Lauryl Sulphate) and achieved an average of 68% COD removal from the car wash wastewater using *Phragmites australis*, a sustainable species in a subsurface flow constructed wetland. Many biomass-based adsorbents satisfying green technology and suitable for surfactant removal are already listed in Table 1.

4.3 Techno-Economic Analysis

Using synthetic (e.g., nanosized) materials for pollutant removal makes adsorption techniques distinctive. Because of their low cost and ease of use, modified clay minerals and biochar have shown excellent potential for eliminating organic and heavy metal pollutants from drinking, industrial, and eutrophic wastewater, despite activated carbon being the most widely used adsorbent (Han et al., 2019). Biochar can absorb physicochemical pollutants like surfactants, costing 60% less than granular activated carbon (GAC) (Kumar et al., 2018). James and Ifelebuegu (2018) researched a few inexpensive, environmentally friendly materials for detergent treatment and removal. Activated carbon (19–2.5 \$ kg⁻¹), silica gel (1–1.5 \$ kg⁻¹), mussel shells (1.5–2.3 \$ kg⁻¹), and zeolite (1.5–2.2 \$ kg⁻¹) are among the biomasses that are promising and potentially sustainable adsorption materials for the reclamation of grey water, according to this study. The commercial price of some easily accessible biomass and mineral adsorbents, such as chitosan (5–10 \$ kg⁻¹), red mud (0.025 \$ kg⁻¹), bagasse fly ash (0.02 \$ kg⁻¹), and carbonaceous adsorbent from fertilizer industry waste (0.1 \$ kg⁻¹), reclaims these materials as sustainable, cost-effective, and potential adsorbents for wastewater treatment (De Gisi et al., 2016). Adsorption is therefore a relatively inexpensive and environmentally benign technique for removing surfactants. Still, it has to be improved further by using new, innovative, environmentally friendly, and easily accessible biomass adsorbents. The degradation of surfactants with a single application of adsorbent is problematic and is hence a

Table 1 Adsorbents and their modifications for surfactant removal

Type of Adsorbents	Materials with their modifications	Type of Wastewater or Surfactant Removed	Results	References
Carbon-Based Adsorbents	Sludge-derived Biochar (SBC) activated by peroxy monosulfate (PMS)	Triclosan surfactant TCS	TCS (0.034 mM) degradation; pH≈7, 0.99 g L ⁻¹ of SBC; 0.8 mM concentration of PMS at 25°C	Wang & Wang, 2019
	<i>Citrus macroptera</i> peels (CMPs) Biochar	Textile wastewater	Adsorption capacity (qm) 139.7 mg L ⁻¹	Roy et al., 2022
	Carbon nanotubes (CNTs)	DDBAC-Dodecyl dimethyl benzyl ammonium chloride, TDBAC-tetradecyl dimethyl benzyl ammonium chloride, CTAB-hexadecyl trimethyl ammonium bromide	All CNTs have 100% removal efficiency for TDBAC (exception OH-MWCNTs). For DDBAC, only SWCNTs have 100% removal efficiency. R_{eff} of CTAB by Pristine MWCNTs with diameter (outer) OD<8 nm is around 50.5 %, while that by OH-WCNTs with OD<8nm is nearly 22.8%.	Gao et al., 2020
	Activated carbon cloth (ACC)	BS - Benzene Sulphonates, TS- <i>p</i> -toluene, OBS-4-octylbenzene, DBS-4-dodecylbenzene	Kinetic model parameters for surfactant adsorption on ACC obtained by linear regression analysis showed $r^2 > 0.999$ for pseudo-2nd-order and $r^2 \approx 0.95$ for pseudo-1st-order. BS < TS < DBS~OBS.	Ayranci & Duman, 2007
	Activated carbon cloth (ACC)	Ammonium chloride of Benzyl trimethyl (BTMACl), benzyl triethyl (BTEACl), benzyl tributyl (BTBACl), benzyl dimethyl decyl (BDMDDACl), benzyl dimethyl tetradecyl (BDMTDACl), benzyl dimethyl hexadecyl (BDMHDACl), and pyridinium chloride of N-dodecyl (N-DPCl) N-cetyl (CPCl)	All surfactants almost complete removal (>98%) (Exception BTMACl, BTEACl) Minor adsorption of BTMACl and BTEACl due to their lesser hydrophobicity than the others.	Duman & Ayranci, 2010
	Powdered activated carbon (PAC)	Linear alkyl benzene sulfonate (LBAS); CTAB	For CTAB and LABS, maximal sorption was observed at around 1.1 and ≈0.499 mmol g ⁻¹ , respectively.	Basar et al., 2004
	Activated carbon (AC)	Mixtures of cationic and anionic surfactants: dodecyl pyridinium chloride-sodium octane sulfonate (DPC-SOS) and octyl triethylammonium bromide-sodium dodecyl benzene-sulfonate (OTEAB-SDBS)	Isotherms showed the presence of 4.0 mmol dm ⁻³ SOS decreases the adsorption of DPC, whereas presence of 0.5 mmol dm ⁻³ OTEAB reduces the adsorption of SDBS	Xiao et al., 2005
	Dolochar from industrial waste	Sodium dodecyl sulfate (SDS)	A removal rate of 98.91% for SDS observed with the optimal settings of adsorbent dosage≈16.6 g L ⁻¹ , contact times≈40 min, initial concentrations≈47 mg L ⁻¹	Shami et al., 2020
	Coconut/coal-based steam-activated carbons; Wood-based, acid-activated carbons	Octanoic acid and dodecanoic acid (C8- and C12-acid)	Amount of C12 adsorbed >> C8 for a common adsorbent and solution phase. The amount of surfactant adsorbed and the adsorbent oxygen content are correlated. Steam-activated carbon(A) > adsorption than phosphoric acid-activated carbon (C)	Wu & Pendleton, 2001
	Multi-walled carbon nanotubes (MWCNT)	Triton (TX-100), CTAB and SDBS	Optimal values for TX-100, SDBS and CTAB are pH= 6, 2 and 8; temperature between 35 to 45°C; removal capacities= 359, 312, and 156 mg g ⁻¹ , respectively	Ncibi et al., 2015
Other Adsorbents	Fly ash of local coal thermal power plant	SDBS	SDBS adsorption was most effective with an adsorbent dose of ≈9.99 g L ⁻¹ and a contact period of around 4.30 hours. A maximum adsorption capacity of 6.83 mg g ⁻¹ was achieved	Siyal et al., 2018
	Commercial carbons Ceca AC40 (C), Merck (M), Sorbo-Norit (S), Almond shells carbon (A)	SDBS	Adsorption capacity calculated by Langmuir equation (for SDBS) on C= 322.4 mg g ⁻¹ M= 348.1 mg g ⁻¹ S= 265.4 mg g ⁻¹ A= 468.8 mg g ⁻¹	Bautista-Toledo et al., 2008
	Novel substrate hydro-thermal processing of fly ash and TiO2	1-hexadecyl trimethyl ammonium bromide-HTAB; SDBS	As per pseudo-2nd-order kinetics, (Cd ²⁺ + SDBS) adsorption is 125.0 mg g ⁻¹ , (Cd ²⁺ + HTAB) is 123.4 mg g ⁻¹	Visa & Duta, 2013
	Degussa P25 nano-powder			
	Coal fly ash (CFA) thermal power plants	SDS	Using ≈99.9 g L ⁻¹ of CFA, the capacity of SDS removal is around 97%.	Zanoletti et al., 2017

Table 1 (continued)

Type of Adsorbents	Materials with their modifications	Type of Wastewater or Surfactant Removed	Results	References
Carbon-Based Adsorbents	Powdered active carbon (PAC)	CTAB	As the equilibrium concentration of CTAB rises to 328 or 348 K, with 18 and 14 mV Zeta potential values of carbon particles	Gurses et al., 2003
	Grafting of arene diazonium salt Phenyl tetra ethylene glycol (PTEG) on Graphene Oxide (GO)	TX-100; Cetyl trimethyl ammonium bromide (DTAB)	The highest removal capacities of GO-PTEG for TX-100 and DTAB were around 1690 and 714 mg g ⁻¹ .	Cheminski et al., 2019
	Activated carbon (AC) obtained from leftover coffee dreg	Primary and secondary sewage wastewater	Turbidity and surfactants were reduced by around 94% and 95%	Marcelo & Alexandre, 2021
Nanomaterial-Based Adsorbents	K ₂ CO ₃ and KOH (activation agents AA), chemically activated carbon (AC) from pine tree cone biomass	SDBS	K ₂ CO ₃ saturation ratio of 0.75 wt% min and max adsorption capacity and removal efficiency are (≈36 mg g ⁻¹ , 35% for w/o AA) and (≈98 mg g ⁻¹ , 95% for AC)	Valizadeh et al., 2016
	Mesoporous nanomaterial MCM-41	CTAB	Surfactant removal by MCM-41, processing time decreased from 14 hrs (calcination) to 5 min (microwaves) saving 72% energy.	López-Pérez et al., 2020
	Graphene oxide (GO); Reduced graphene oxide (rGO) nanomaterials	TX-100	Exclusion capacities of 1683 mg g ⁻¹ for rGO; 1203 mg g ⁻¹ for GO after 3 removal cycles adsorption capacity of rGO ≈1050 mg g ⁻¹ .	Prediger et al., 2018
	Zero-Valent Iron (nZVI)	Hexadecyl pyridinium chloride surfactant (HDPCL); SDBS	Removal efficiency of HDPCL ≈ 99% and of SDBS ≈93 %	Abd El-Lateef et al., 2018
	Nanoporous nickel phosphate (nano-NiPOx) particles	Cetylpyridinium chloride (CPC)	NIPOx shows max adsorption of 360.5 mg g ⁻¹ for CPC	Touny et al., 2019
Biomass-Based Adsorbents	Chitosan	SDBS	Maximum effectiveness of SDBS removal is 97.3 % at pH 4 with adsorbent dose 0.5 g, initial SDBS concentrations 25 mg L ⁻¹ , at 25°C and 60 min, adsorption of 6.38 mg g ⁻¹ .	Pahizgar et al., 2017
	Corn cob Adsorbents	Anionic Surfactants	Nearly 97 % COD; 97.4 % BOD; 72 % Phosphate; 81.68 % Ammonia and 92 % Surfactant were removed	Priyanka et al., 2020
	Chromium-containing leather waste	SDBS, Cationic-- dodecyl trimethyl ammonium bromide (DTB) and TX-100	Poor adsorption of DTB, TX-100 on Cr- Leather. Adsorption capacity of SDBS increased with temperature, reaching its highest at 293 K at 375 mg g ⁻¹ and its highest at 313 K at 423 mg g ⁻¹ .	Mi-Na et al., 2006
	Rice husk-derived biochar (RHB)	Shipboard bilgewater (SBW) Sodium dodecyl sulfate	Optimal conditions with surfactant removal efficiency 96.6 %; flow rate- 5 mL min ⁻¹ ; bed depth-16 cm gives	Dadebo et al., 2023
	Citrus macroptera peels biochar	Synthetic wastewater	Maximum adsorption capacity, qm was 139.7 mg g ⁻¹ .	Roy et al., 2022
	<i>Artocarpus heterophyllus</i> seed powder	Residential laundry wastewater	Removal efficiency for surfactants ≈ 92%, COD ≈83%, BOD ≈78%, and turbidity ≈85%, optimal initial pH 6, a dose of 2.5 g L ⁻¹ , and duration of ≈ 30 min	Deressa et al., 2019
	Crosslinked biopolymer-based Chitosan Films	SDBS	High adsorption capacity (qm) for SDBS ≈ 714 mg g ⁻¹ at pH= 2, 180 min.	Kahya et al., 2018
	Chitosan hydrogel beads	SDS	As per Langmuir adsorption isotherm SDS adsorption (Qmax ≈ 77 mg g ⁻¹)	Pal et al., 2013
	Amino crosslinked chitosan microspheres (ACCMs)	SDBS, SDS and sodium lauryl sulfate (SLS)	Adsorption saturation for ACCMs for SDBS ≈1219 mg g ⁻¹ , SLS ≈890 mg g ⁻¹ , and SDS ≈824 mg g ⁻¹ at pH 3.0 and around 300 K.	Zhang et al., 2017
	<i>Strychnos potatorum</i> seeds and activated carbon from <i>Colocasia esculenta</i>	Laundry Wastewater	Reduction in total dissolved solids from 168 ppm to 12 ppm (≈ 93% reduction), and turbidity lowered from 132 NTU to 10 NTU	Sriram, 2019

Table 1 (continued)

Type of Adsorbents	Materials with their modifications	Type of Wastewater or Surfactant Removed	Results	References
Polymer	Polyvinyl alcohol (PVA) and polyacrylic acid (PAA)	Tetradecyl poly-oxy-ethylenated monolaurate [La (EO) ₁₄] ⁺ tetradecyl poly oxy ethylenated monooleate [Ol (EO) ₁₄] ⁺	Amount adsorbed (m mol g^{-1}) = 0.2020; 0.0730 on PAA and 0.065; 0.050 on PVA. Equilibrium concentration, $C_{\text{eq}} \times 10^3 \text{ mol dm}^{-3} = 0.039$; 0.070 on PAA and 0.051; 0.040 on PVA. Minimum area occupied by surfactant on the polymer, $A_{\text{min}} (\text{\AA}^2) = 0.82$; 2.27 on PAA and 2.59, 3.32 on PVA.	El-Feky et al., 2009
Mineral or Clay (Others)	Poly (ethylene glycol) poly (ethylene) block copolymers	SDS, Disponil AFX 1080	Langmuir Isotherm $K [\text{m}^3 \text{mol}^{-1}] = 0.064 \pm 0.002$ for (SDS), and 7.4 ± 1.2 for Disponil AFX 1080. $a_{\text{cmc}} [\text{\AA}^2] = 29 \pm 5$ for (SDS), and 24 ± 9 for Disponil AFX 1080.	Meconi et al., 2016
	Organic resin (Lewatit VPOC 1064 MD PH)	CTAB, SLES (sodium dodecyl ether sulfate)	Max removal of adsorbate is around 11 times > for SLES than for CTAB.	Gönder et al., 2010
	Fly ash-based geopolymer (FAGP)	SDBS	Optimal parameters pH 2, 180 min of contact, 1 g L^{-1} adsorbent dosage. Max adsorption capacity $\approx 715 \text{ mg g}^{-1}$; activation energy $\approx 4.05 \text{ kJ mole}^{-1}$.	Siyal et al., 2019
	Sandstone with Ca-montmorillonite kaolinite clays	Alkyl ethoxy carboxylate (AEC) for Enhanced Oil Recovery (EOR)	Sandstone with 15% Ca-montmorillonite and kaolinite clay has lower surfactant adsorption than at 10% and 25% concentrations.	Herawati et al., 2022
	Chilean zeolite modified with CTAB -cetyl trimethyl ammonium bromide	SDBS	Maximum adsorption capacity of SDBS is $\approx 31 \text{ mg g}^{-1}$ at CTAB loading of 660% external cation exchange capacity.	Taffarel & Rubio, 2010
	Granite sand	Triton X-100	Adsorption TX-100 = $2.16 \times 10^{-4} \text{ g g}^{-1}$; temp = 32°C ; pH ≈ 6 ; amt of sand = 7.0 g; time = 15 min	Khan & Zareen, 2004
Natural zeolite	α -Alumina (Al_2O_3) beads	SDS	SDS adsorption (pH=4) For 0.001 C (M NaCl); $\Gamma^\infty = 1.20 (\text{mmol m}^{-2})$; For 0.01 C (M NaCl); $\Gamma^\infty = 1.55 (\text{mmol m}^{-2})$; For 0.1 C (M NaCl); $\Gamma^\infty = 1.67 (\text{mmol m}^{-2})$	Pham et al., 2015
	Natural zeolite	SDS; CTAB	CTAB has a larger adsorption capacity on zeolite than SDS, with capacities of 284 mg g^{-1} and 113 mg g^{-1} , respectively.	Harunyan & Pirunyan, 2015

leading drawback of adsorption. An admirable strategy for improving surfactant removal and process cost-effectiveness would be blending with other removal methods that tend to degrade.

4.4 Industrial Applications and Future Advances

The successful removal of synthetic surfactants from industrial wastewater ($\approx 99.9\%$) was exhibited by a hybrid ion exchange fibre material (FM) that improved its operational cycle to 200 L. A hybrid ion exchange FM with both anion-active (A-FM) and cation-active matrices (C-FM) was created by blending different ratios. In four sorption columns with varying ion-exchange fibre material compositions, working life tests of the hybrid IFM were carried out concurrently. These columns processed industrial wastewater at a rate of 0.13 L min^{-1} , pre-purified on a ceramic membrane. Hybrid ion exchange FM, utilized in the ratio of C-FM (3): A-FM (7), achieved the highest and most steady degree of purification (Artemenko et al., 1997).

Recently, a study revealed the efficiency of Iraqi reed (IR) as a biomass precursor for IRAC synthesis and anionic surfactant removal from industrial wastewater. Iraqi reed (IR) biomass waste was recently processed into activated carbon (AC) using a pyrolysis-assisted H_3PO_4 activation process. In contrast to the IR surface area of $0.5542 \text{ m}^2 \text{ g}^{-1}$, the BET surface area significantly increased upon pyrolysis. SDBS a model anionic surfactant, was eliminated using Iraqi reed-activated carbon (IRAC). The adsorption kinetics and equilibrium data demonstrated that SDBS adsorption follows the pseudo-second-order and Langmuir models under kinetic and equilibrium conditions. The maximum adsorption capacity for SDBS was 121.5 mg g^{-1} (Ahmed et al., 2023).

Zeolites can eradicate many organic pollutants, including cationic surfactants. Zeolites are employed in various applications because of their appreciable capacity for cation exchange, specific surface area, and lattice stability. The tendency of reversible sorption in zeolites makes them reusable. Nano-zeolites (N-Zeo), inorganic-N-Zeo composites, polymer-N-Zeo composites, and zeolite-nanoparticle composites have all been developed to eliminate pollutants like surfactants using sorption or ion exchange batch techniques (Rahman et al., 2022). Innovative materials like β -cyclodextrin-functionalized coffee husk

biochar (de Benedicto et al., 2024), activated carbon obtained from waste tires (Ramírez-Arias et al., 2020), pine wood activated carbon (Azoulay et al., 2023), metal oxides using quartz crystal microbalance with dissipation (Medina et al., 2020) are a few of the recent advances in surfactant adsorption.

Fortifying new materials for the enhancement of adsorbents can be helpful for improved adsorption of surfactants on their surface. Various chemicals, nanoparticles, biomaterials and minerals modify the adsorbents (Liu et al., 2021; Zhou et al., 2018). Developing new composites from such modifications is an emerging field in surfactant adsorbents. The following section discusses the employment of such composite adsorbents for surfactant removal. Figure 2 illustrates the mechanism of surfactant adsorption through fortifying adsorbents for composite formation.

5 Composites for Surfactant Removal

Advanced technologies such as photo-catalysis, Fenton, electro-Fenton, adsorption, and catalytic ozonation processes have employed metal composites based on biochar (BC) due to their good efficiency and cheaper cost. These metal composites have also been used to break down surfactants (Ahmad et al., 2022). Composite adsorbents appear to be a better option than normal adsorbents since they combine two or more components, imparting strong adsorbent ability to the resultant material, cost reduction and are readily available (Aguilar-Bolados et al., 2019). Water pollution is a significant issue in the modern era, and research relies on building effective polymeric adsorbents and membranes. The fabrication of polymeric nanocomposites that are non-toxic, biocompatible, economical, and effective continues to be explored, though. The use of nanofillers or nanoparticles enhances the mechanical, thermophysical, and physicochemical properties of these nanocomposites. Methods of fabrication and enhancement include mixing, in-situ polymerization, melt-mixing, electrospinning, and selective laser sintering. Emerging technologies strive to create polymer nanocomposites that are efficient, long-lasting, and profitable, with uniform dispersion and minimum errors. Polymer nanocomposites serve as adsorbents and filter membranes to remove organic pollutants and surfactants from aqueous media (Adeola & Nomngongo, 2022).

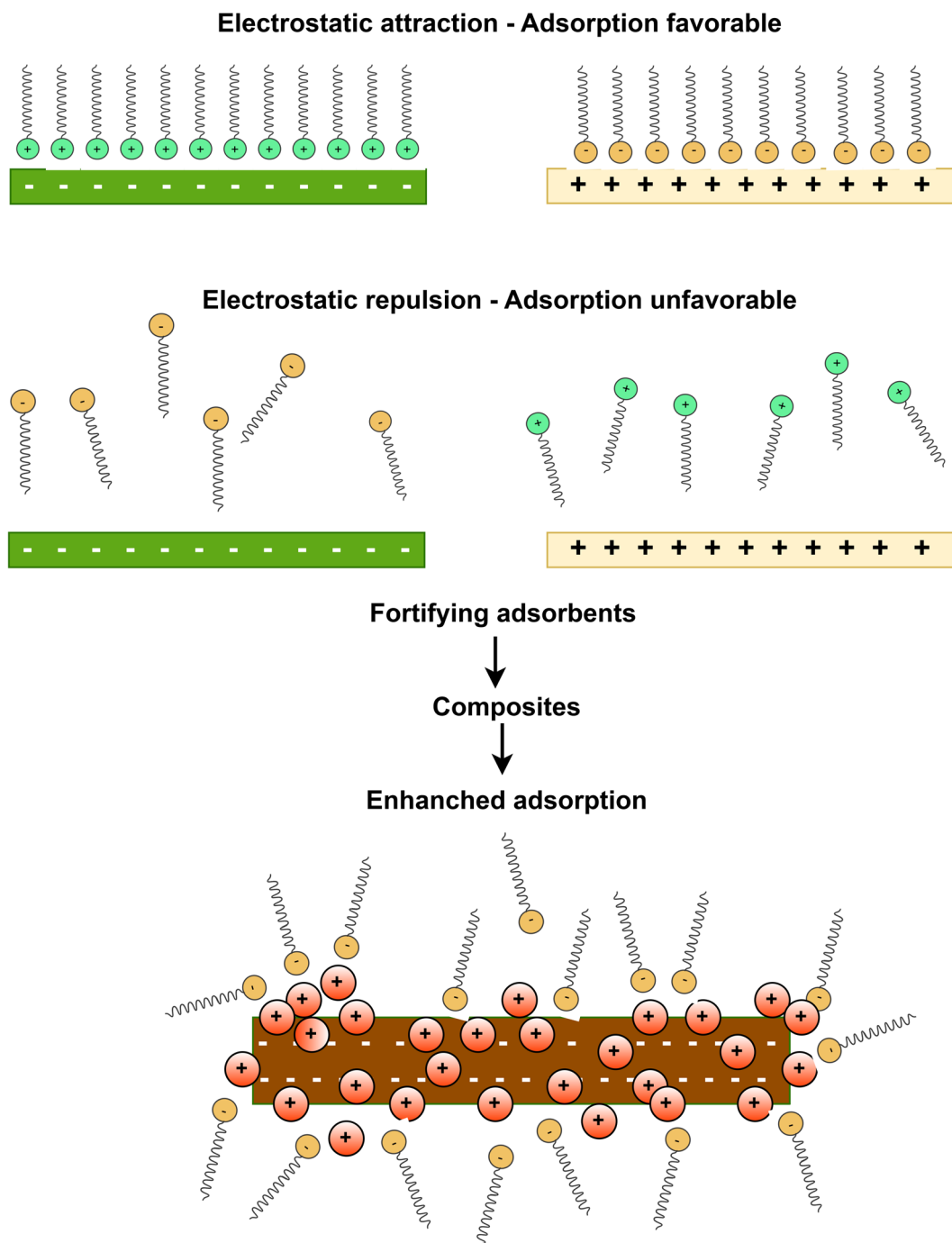


Fig. 2 Fortifying adsorbents for composite formation

Figure 3 illustrates various adsorbent materials used in composites for surfactant removal. Composites can facilitate better, cheaper, and eco-friendly adsorption processes for easy pollutant removal from wastewater.

Designing a composite based on the requirements of functional groups, cheaper biomass with easy availability and disposal ability is currently being explored to the maximum.

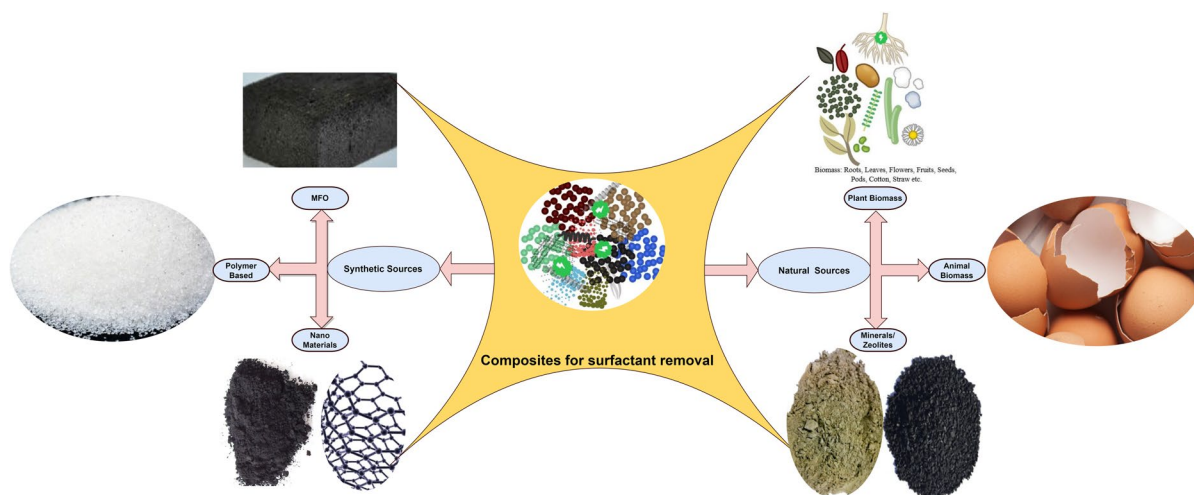


Fig. 3 Adsorbents for composites

A composite of PEI-PVA nanospheres was developed by combining polyvinyl alcohol (PVA) with polymer polyethyleneimine (PEI). This combination applied a series of chemical changes, utilizing the adequate oxygen-containing functional groups on the PVA surface. Under acidic and alkaline conditions, PEI-PVA composite nanospheres showed admirable adsorption effects for anionic surfactants in the wastewater. The adsorption capacity increased as the treatment duration was extended, eventually stabilizing after 24 hours (Liu et al., 2023). Some composites for surfactant removal to date have been enlisted in Table 2.

6 Future Perspectives

Membrane filtration, coagulation, flocculation, and sedimentation are the standard pre-treatment processes that selectively remove harmful pollutants from wastewater units. Though these approaches are practical for surfactant removal, they unavoidably raise overall operating costs and environmental impact. Subsequently, the future opportunity rests in making them cheaper and more environmentally friendly. Hence, hybrid approaches can be helpful

for surfactant removal in addition to obligating the least energy, labour, and operating costs.

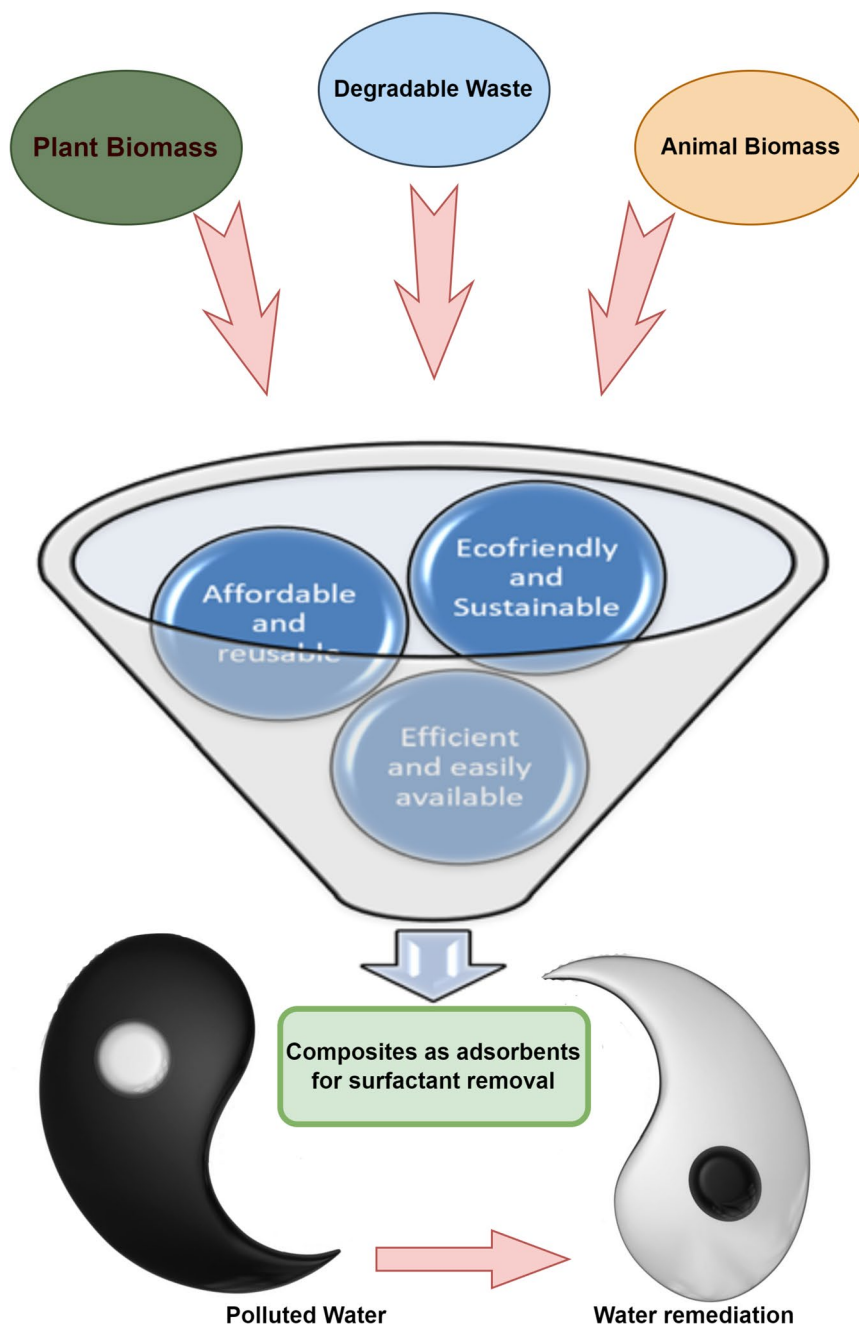
Green adsorbents as composites appear to be a better option in this consideration. Exploring more agricultural wastes as surfactant adsorbents is necessary to sustain the market for adsorbent composites while lowering production costs (Faccenda et al., 2021). Enhancing the processability of biomass feedstock (Ramírez-Arias et al., 2020) and pretreatment methods to make it more suitable for use as an adsorbent in surfactant removal will be advantageous. Degradable waste material is another aspect that needs to be explored while designing composites. An amalgamation of low-cost biosorbent carriers with polymers, minerals, nano adsorbents or other materials to increase bulk production at low cost can be explored. Figure 4 portrays an ideal composite design for surfactant removal during water remediation.

Investigating novel functional materials and developing hybrid technologies can improve the surfactant adsorption efficiency of composites. Improving composites under various optimal environmental circumstances by thoroughly examining the adsorption mechanism to comprehend the science underlying the surfactant adsorption behaviors is essential.

Table 2 Composites for surfactant removal

Sr.No.	Composite Material Used	Surfactant Removed or Type of Wastewater	Results	References
1.	Carboxylated carbon nanotubes (CCNT)-TiO ₂ loaded onto polyethyleneimine-chitosan aerogel (PCA) CCNT-TiO ₂ @PCA	SDBS	Surfactant removal rate > 91%. Max adsorption capacity of CCNT- TiO ₂ @PCA ≈ 3155 mg g ⁻¹	Fan et al., 2023
2.	Lignite (LIG)-Bentonite (BEN) composite (BL)	SDBS	SDBS adsorbed on LIG (80.77 g kg ⁻¹) BEN (18.32 g kg ⁻¹)	Solińska et al., 2023
3.	β-FeOOH-SBA-15 composites	Nonionic Surfactant P123	The triblock copolymer P123 could be efficiently removed by treatments at 40–80 °C for one–three hours,	Huang et al., 2023
4.	Eggshell-zeolite composite	Handwashing wastewater	COD removal rate = 88%, surface area = 95 mg g ⁻¹ , pore width = 10 nm, methylene blue number = 26 m ² g ⁻¹	Turyasingura et al., 2023
5.	Magnetic carbon nanocomposite (MCNC)	CTAB	Retention≈99.99% (no effect on permeate flux) of the RO membrane with MCNC pretreatment	Ali et al., 2019
6.	Polymeric Microporous adsorbents (CAD-100 and CAD-200) using bentonite composite adsorbent (BKA)	Textile wastewater, Anionic surfactant	Reduction of COD= 65 % and concentration of surfactant=82 %,	Amonova & Ravshanov, 2019
7.	Magnetic nanocomposite sorbents (Saponite, palygorskite, and sponylite clay)	SDBS, SLS and polyphosphates	Surfactants and polyphosphate removal is 2–8 times higher than native clay.	Makarchuk et al., 2017
8.	Kaolinite clay mineral composite (KCC)	SDBS	At pH 4, adsorbent doses (0.5 g), and temperatures (30°C), KCC was able to remove 71% of SDBS in just 60 min	Kamal et al., 2017
9.	Porous membrane-based composite (PS-GO) Polysulfone (PS); graphene oxide (GO)	Triton X 100	After 4 hours treatments; removal efficiency > 90%	Zambianchi et al., 2017
10.	Fly ash TiO ₂ composite	SDBS	78% of the SDBS surfactant was removed	Visa et al., 2015
11.	Chemically crosslinked composite gels - bentonite clay and nonionic polymers	CTAB and cetyl pyridinium bromide (CPB)	Surfactant adsorption causes shifts of critical micelle concentration (CMC) from 500 µl to 720 µl	Beisebekov et al., 2015
12.	Geomaterial composite formed by bentonite (mostly Ca-montmorillonite) and activated carbon.	Dodecylbenzene sulfonic acid surfactant (DBSA)	0.3 g of geomaterial was equally effective in removing LAS as activated carbon and montmorillonite at concentrations 7 and 10 times higher, respectively	Mimame et al., 2012
13.	Commercial DL composite membrane	Chemipur CL80	Removal efficiency > 94%, at lower temp, higher removal efficiency achieved > 97 %, greatest surfactant removal attained at 20°C temperature, pressure- 40 bar.	Kertész et al., 2008
14.	Bentonite and <i>Duranta erecta</i> fruit powder mixer embedded alginate beads	CTAB	Beads CTAB adsorption capacity qm values = 2862–2352 mg g ⁻¹	Golder et al., 2021
15.	Graphene oxide (GO)-enhanced composite metal-organic frameworks (MOF)	Carwash wastewater	Effective surfactant removal ≈91% to 97%. Surfactant adsorption capacity (24.48 mg g ⁻¹)	Mklima et al., 2024

Fig. 4 Designing an ideal composite for surfactant removal



7 Conclusion

A concrete and assured surfactant removal materials and methodologies are still lacking. Efficacious commercialization and field-scale application of carbon-based adsorbents for surfactant removal in wastewater treatment require addressing several limitations. Energy-intensive synthesis restricts

large-scale production, necessitating the development of low-cost technologies for activated carbon synthesis. The low conductivity, limited adsorption capacity, and low stability of raw biochar are some of its limitations, which make its modification essential. The synthesis of magnetic biochar composite can aid in the retrieval and reusability of biochar. Upcoming research should also explore the risk of

secondary contamination to evaluate the sustainability of carbon-based technologies for real-world applications of surfactant removal. The utility of photocatalysts like TiO_2 combined with various adsorbents in hybrid techniques for surfactant removal needs modifications. Due to their significant band gaps, these photocatalysts can access significantly less of the solar spectrum in the photocatalytic process; hence, they need to reduce the band gap for appropriate electronic excitation. Novel yet biodegradable polymer adsorbent and some waste disposal adsorbent materials as composites need to be explored. Future studies should concentrate on combining nano adsorbent materials with bio-sorbent carriers, investigating novel functional materials, and enhancing the adsorbents' selectivity and operating expenses for surfactant mitigation. Though some composites facilitate surfactant removal, their real-time application still seems complicated. Developing hybrid surfactant removal technologies and adsorbents from composite or mixed biomass sources can be used in real-field applications, requiring further research.

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Dipika Jaspal: Critical revision, Guiding, Proofreading, Supervision.

Nilisha Itankar: Guiding, Supervision.

All authors read and approved the final manuscript.

Declarations

Competing Interests The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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